

Lecture 22: Ideal Fluids

- Logistics:
- PS8 due
 - PS5 graded
 - Try to post new one

Last time: - Isotropic tensor functions

$$\underline{\underline{G}}(\underline{\underline{A}}) = \alpha_0(\underline{\underline{I}}_A) \underline{\underline{I}} + \alpha_1(\underline{\underline{I}}_A) \underline{\underline{A}} + \alpha_2(\underline{\underline{I}}_A) \underline{\underline{A}}^2$$

- linear isotropic

$$\underline{\underline{G}}(\underline{\underline{A}}) = \underline{\underline{C}} \underline{\underline{A}} = \lambda \text{tr}(\underline{\underline{A}}) \underline{\underline{I}} + 2\mu \text{sym}(\underline{\underline{A}})$$

- 4th order tensors

$$\underline{\underline{C}} = C_{ijkl} \underline{e}_i \otimes \underline{e}_j \otimes \underline{e}_k \otimes \underline{e}_l$$

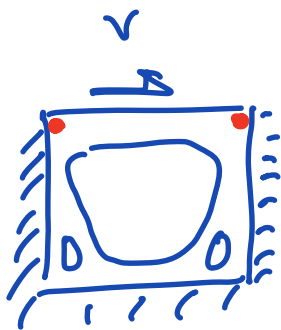
$$C_{ijkl} = \underline{e}_i \cdot \underline{\underline{C}} (\underline{e}_k \otimes \underline{e}_l) \underline{e}_j$$

$$\underline{\underline{U}} = \underline{\underline{C}} \underline{\underline{A}} \quad U_{ij} = C_{ijkl} A_{kl}$$

- Material constraints $\gamma(\underline{\underline{E}}) = 0$

$$\underline{\underline{E}} = \underline{\underline{E}}^r + \underline{\underline{E}}^a$$

p is multiplier that enforces γ



Today: Ideal Fluids.

Isothermal Fluid Mechanics

→ application of Eulerian balance law

$$\nabla_x = \nabla$$

→ neglect thermal effects

10 equations

$$\underline{v}_m = \dot{\varphi} \quad 3 \text{ kinematic}$$

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \underline{v}) = 0 \quad \text{mass balance}$$

$$\rho \dot{\underline{v}} = \nabla \cdot \underline{\underline{\sigma}} + \rho \underline{b} \quad 3 \text{ lin. mom}$$

$$\underline{\underline{\sigma}} = \underline{\underline{\sigma}}^T \quad 3 \text{ ang. mom}$$

$$16 \text{ unknowns: } \begin{matrix} \varphi \\ 3 \end{matrix} \quad \begin{matrix} \underline{v} \\ 3 \end{matrix} \quad \begin{matrix} \rho \\ 1 \end{matrix} \quad \begin{matrix} \underline{\underline{\sigma}} \\ 9 \end{matrix} = 16$$

⇒ Constitutive relation that relates

6 independent comp. $\underline{\underline{\sigma}}$ to \underline{v}

Material constraint: add both 1 equ ($\gamma(\underline{\underline{\sigma}}) = 0$)
and 1 unknown multiplier q .

Ideal fluids

A fluid is ideal if

1) Uniform ref. mass density: $\rho_0(\underline{x}) = \rho_0 > 0$

2) Incompressible: $\nabla \cdot \underline{v} = 0$

3) Cauchy stress is spherical: $\underline{\underline{\sigma}} = -p \underline{\underline{I}}$

\Rightarrow no shear stress $\underline{t} = \underline{\underline{\sigma}} \underline{n} = -p \underline{n}$

1 + 2 $\Rightarrow \rho(\underline{x}, t) = \rho_0$

Subst. into mass balance

$$\cancel{\frac{\partial \rho_0}{\partial t}} + \nabla \cdot (\cancel{\rho_0} \underline{v}) = 0 \quad \Rightarrow \quad \boxed{\nabla \cdot \underline{v} = 0}$$

continuity eqn

Subst. into mom. balance

$$\rho_0 \dot{\underline{v}} = -\nabla \cdot (p \underline{\underline{I}}) + \rho_0 \underline{b}$$

expand mat. deriv $\dot{\underline{v}} = \frac{\partial \underline{v}}{\partial t} + (\nabla \underline{v}) \underline{v} + (\underline{v} \cdot \nabla) \underline{v}$

Closed sys. of eqns for \underline{v} & p

$$\boxed{\begin{aligned} \frac{\partial \underline{v}}{\partial t} + \underline{(\nabla \underline{v}) \underline{v}} &= -\frac{1}{\rho_0} \nabla p + \underline{b} \\ \nabla \cdot \underline{v} &= 0 \end{aligned}}$$

Euler Equations

4 eqns for 4 unknowns

Note: p has an undetermined constant.

Frame-indifference of Euler's eqns

Stress field in ideal fluid is entirely reactive

$$\underline{\underline{\sigma}} = \underline{\underline{\sigma}}^r - \underline{\underline{\sigma}}^a = -p \underline{\underline{I}}$$

$$\underline{\underline{\sigma}}^r = -p \underline{\underline{I}} \quad \underline{\underline{\sigma}}^a = \underline{\underline{0}}$$

here p is multiplier cons. with incomp. const.

For constrained model we just need to show

that $\underline{\underline{\sigma}}^a$ and $\gamma(\underline{\underline{F}}) = 0$ are frame-indifferent.

Assuming a superpose rigid motion

$$\underline{\underline{x}}^* = Q(t) \underline{\underline{x}} + \underline{\underline{c}}(t)$$

$$\begin{aligned} \bullet \gamma(\underline{\underline{F}}^*) &= \det(\underline{\underline{F}}^*) - 1 = \det(Q \underline{\underline{F}}) - 1 = \det(Q) \det(\underline{\underline{F}}) - 1 \\ &= \gamma(\underline{\underline{F}}) \quad \checkmark \end{aligned}$$

$$\bullet \underline{\underline{\sigma}}^a = \underline{\underline{0}} \quad \text{trivially frame-indifferent}$$

\Rightarrow Ideal fluid material model is frame-indif.

Mechanical energy considerations

Even in isothermal model the entropy inequality provides a constraint on material model.

Lecture 18: $\rho_0 \dot{\psi} \leq \underline{\underline{\sigma}} : \underline{\underline{d}}$ Mech. Energy Ineq. (MEI)

where $\underline{\underline{\sigma}} : \underline{\underline{d}} = -p \underline{\underline{I}} : \text{sym}(\nabla \underline{\underline{v}})$

use $\underline{\underline{I}} : \underline{\underline{A}} = \text{tr}(\underline{\underline{A}})$ & $\text{tr}(\text{sym}(A)) = \text{tr}(A)$

$$\Rightarrow \underline{\underline{\sigma}} : \underline{\underline{d}} = -p \text{tr}(\nabla \underline{\underline{v}}) = -p \nabla \cdot \underline{\underline{v}} = 0$$

In an ideal fluid stress power vanishes

$\dot{\psi} = 0$ Free energy is constant

Steady Bernoulli Streamline Theorem

From PS4: $(\nabla \underline{\underline{v}}) \underline{\underline{v}} = (\nabla \times \underline{\underline{v}}) \times \underline{\underline{v}} + \frac{1}{2} \nabla |\underline{\underline{v}}|^2$

subst into mom. bal.

$$\frac{\partial \underline{\underline{v}}}{\partial t} + (\nabla \times \underline{\underline{v}}) \times \underline{\underline{v}} = -\frac{1}{\rho_0} \nabla |\underline{\underline{v}}|^2 - \frac{1}{\rho_0} \nabla p + \underline{\underline{b}}$$

for a conservative body force $\underline{\underline{b}} = -\nabla \psi$

where ψ is the force potential.

collecting ∇ on rhs

$$\frac{\partial \underline{v}}{\partial t} + (\nabla \times \underline{v}) \times \underline{v} = -\nabla H$$

$$H = \frac{1}{2} |\underline{v}|^2 + \frac{p}{\rho_0} + \psi \quad \text{for gravity } \psi = gz$$

H has units of Energy/mass

$$E_k = \frac{1}{2} m |\underline{v}|^2 \quad E_g = mgz \quad E_E = m \int_{p_0}^p \frac{dp}{\rho} = m \frac{p - p_0}{\rho}$$

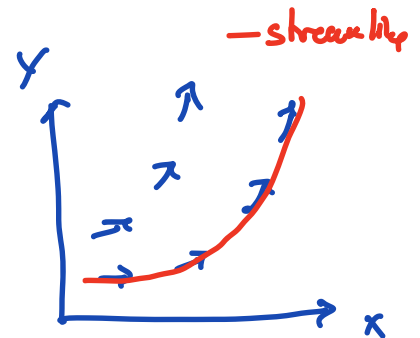
$$H = \frac{E}{m} = \frac{E_k}{m} + \frac{E_E}{m} + \frac{E_g}{m} = \frac{1}{2} |\underline{v}|^2 + \frac{p}{\rho_0} + gz$$

Steady flow

$$(\nabla \times \underline{v}) \times \underline{v} = -\nabla H$$

take dot product from left

$$\underline{v} \cdot \underbrace{(\nabla \times \underline{v}) \times \underline{v}}_{\perp \underline{v}} = -\underline{v} \cdot \nabla H$$



\Rightarrow $\underline{v} \cdot \nabla H = 0$ Bernoulli's Theorem for steady flow

implies that H is constant along a streamline

Streamline a curve tangent everywhere to \underline{v}

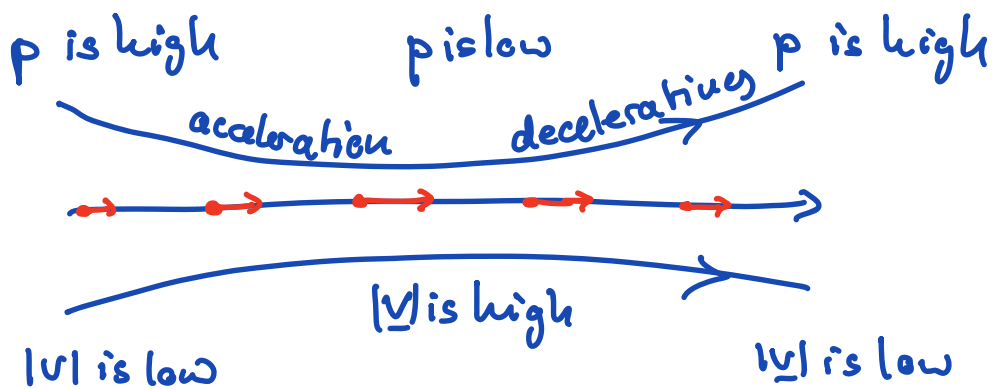
$$\frac{dy}{dx} = \frac{v_y}{v_x}$$

⇒ H is constant along streamlines, because energy is constant $\dot{\psi} = 0$

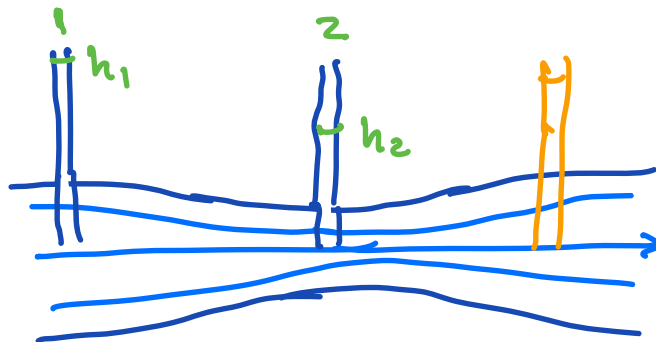
In an ideal fluid there is no energy dissip.

$$H = \frac{1}{2} |\underline{v}|^2 + \frac{P}{\rho_0} + gz = \text{const}$$

if $z = \text{const}$ then increase in \underline{v} requires decrease in P along a streamline



Example: Venturi meter



H is const along along central streamline

$$H = \frac{P_1}{\rho} + \frac{1}{2} v_1^2 = \frac{P_2}{\rho} + \frac{1}{2} v_2^2 \quad (z=0)$$

$$p_0 \quad \dots \quad p_0 \quad z = z \quad \dots \quad \dots$$

from mass balance: $A_1 v_1 = A_2 v_2 \quad v_2 = \frac{A_1}{A_2} v_1$

hydrostatics: $p_1 - p_0 = \rho g h_1 \quad p_2 - p_0 = \rho g h_2$

$$\rho g (h_1 - h_2) = \frac{\rho}{2} \left(\frac{A_1^2}{A_2^2} - 1 \right) v_1^2$$

solve for v_1 :

$$v_1^2 = \frac{2g(h_1 - h_2)}{\left(\frac{A_1^2}{A_2^2} - 1 \right)}$$

Irrotational Motion

\underline{v} is irrotational if

$$\underline{\underline{\omega}} = \text{skew}(\nabla \underline{v}) = \underline{\underline{0}} \quad \text{or} \quad \nabla \times \underline{v} = \underline{\underline{\omega}} = \underline{\underline{0}}$$

particle experience no net rotation.

Velocity potential

Helmholtz decomposition of velocity

$$\underline{v} = \nabla \phi + \nabla \times \underline{\psi}$$

for irrotational flow

$$\nabla \times \underline{v} = + \nabla \times \nabla \phi + \nabla \times \nabla \times \psi = \underline{0}$$

$$\Rightarrow \psi = 0$$

Irrrotational flows have a scalar velocity potential:

$$\underline{v} = + \nabla \phi$$

$$\Rightarrow \nabla \cdot \underline{v} = + \nabla^2 \phi = 0 \quad \text{Laplace Egn}$$

In steady irrotational flow

$$(\nabla \times \underline{v}) \times \underline{v} = -\nabla H$$

$$\nabla H = 0$$

H is constant in a steady-irrotational ideal fluid

Time dependent irrotational flows

Starting from mom. balance

$$\frac{\partial \underline{v}}{\partial t} + (\nabla \times \underline{v}) \times \underline{v} = -\nabla H$$

$$-\nabla \frac{\partial \phi}{\partial t} + \nabla \left(\frac{1}{2} |\underline{v}|^2 + \frac{p}{\rho_0} + gz \right) = 0$$

$$\nabla \left(\frac{\partial \phi}{\partial t} + \frac{1}{2} |\underline{v}|^2 + \frac{p}{\rho_0} + gz \right) = 0$$

This implies

$$\frac{\partial \phi}{\partial t} + \frac{1}{2} |\underline{v}|^2 + \frac{P}{\rho_0} + gz = 0$$
$$\nabla^2 \phi = 0$$
$$\underline{v} = \nabla \phi$$

Bernoulli's Theorem
for irrotational flow

Big simplification but are flows irrotational.

Vorticity equation

vorticity: $\underline{\omega} = \nabla \times \underline{v}$

subst. into mom. bal.

$$\frac{\partial}{\partial t} \underline{v} + \underline{\omega} \times \underline{v} = -\nabla H$$

take the curl

$$\frac{\partial}{\partial t} \underline{\omega} + \nabla \times \underline{\omega} \times \underline{v} = -\nabla \times \nabla H = 0$$

where $\nabla \times \underline{\omega} \times \underline{v} = (\nabla \underline{\omega}) \underline{v} + (\nabla \underline{v}) \underline{\omega} - (\nabla \underline{v}) \underline{\omega} - (\nabla \underline{\omega}) \underline{v}$

$$\frac{\partial}{\partial t} \underline{\omega} + (\nabla \underline{\omega}) \underline{v} - (\nabla \underline{v}) \underline{\omega} = 0$$

$$\underline{\dot{\omega}} - (\nabla \underline{v}) \underline{\omega} = 0$$

Vorticity eqn

Use this to show that an initially irrotational fluid remains irrotational!

Simple proof in 2D:

$$\underline{v} = \begin{pmatrix} v_x \\ v_y \\ 0 \end{pmatrix} \quad \nabla \underline{v} = \begin{pmatrix} v_{x,x} & v_{x,y} & 0 \\ v_{y,x} & v_{y,y} & 0 \\ 0 & 0 & 0 \end{pmatrix} \quad \underline{\omega} = \nabla \times \underline{v} = \begin{pmatrix} 0 \\ 0 \\ \omega \end{pmatrix}$$

$$\Rightarrow (\nabla \underline{v}) \underline{\omega} = 0 \Rightarrow \dot{\underline{\omega}} = \underline{0}$$

Vorticity of fluid element is conserved in ideal fluid.

Vorticity is const. along streamlines

In particular if $\underline{\omega} = 0$ everywhere initially it will remain zero.

\Rightarrow Bernoulli's Theorem for irrotational flows applicable to broad range of problems.

