

Lecture 23: Newtonian Fluids

Logistic: - sorry no new HW

Last time: - Ideal fluids

- spherical Cauchy stress: $\underline{\underline{\sigma}} = -p\underline{\underline{I}}$

Euler Equations

$$\rho_0 \left(\frac{\partial \underline{v}}{\partial t} + \underline{(\nabla_x v) v} \right) = -\nabla_x p + \rho_0 \underline{b}$$

$$\nabla_x \cdot \underline{v} = 0$$

- zero stress power \rightarrow no energy diss.

- Bernoulli theorem

Steady: $\underline{v} \cdot \nabla_x H = 0$

$$H = \frac{1}{2} |\underline{v}|^2 + \frac{p}{\rho_0} + gz$$

Irrrotational: $\underline{v} = \nabla_x \phi$

+ steady $\nabla H = 0$

+ transient $\frac{\partial \phi}{\partial t} + \frac{1}{2} |\underline{v}|^2 + \frac{p}{\rho_0} - gz = f(t)$

- Vorticity equation $\nabla_x^2 \phi = c$

$$\dot{\underline{\omega}} - (\nabla_x \underline{v}) \underline{\omega} = \underline{0}$$

Newtonian Fluid

- 1) Ref mass density $\rho(\underline{x}) = \rho_0$
- 2) Incompressible $\nabla_{\underline{x}} \cdot \underline{v} = 0$
- 3) Cauchy stress is Newtonian

$$\underline{\underline{\sigma}} = -p \underline{\underline{I}} + \mathbb{C} \nabla_{\underline{x}} \underline{v}$$

$p = \text{pressure}$

\mathbb{C} 4th order tensor

\mathbb{C} must have left minor sym. $(\mathbb{C} \underline{\underline{A}})^T = \mathbb{C} \underline{\underline{A}}$

\Rightarrow ensures $\underline{\underline{\sigma}}^T = \underline{\underline{\sigma}} \rightarrow$ ang. mom. balance

$$\text{tr}(\mathbb{C} \underline{\underline{A}}) = 0 \quad \text{if} \quad \text{tr}(\underline{\underline{A}}) = 0$$

$$\Rightarrow p = \frac{1}{3} \text{tr}(\underline{\underline{\sigma}}) \quad \text{when} \quad \text{tr}(\nabla_{\underline{x}} \underline{v}) = \nabla_{\underline{x}} \cdot \underline{v} = 0$$

Prop. 1+2 $\Rightarrow p(\underline{x}, t) = p_0$

Reactive stress: $\underline{\underline{\sigma}}^r = -p \underline{\underline{I}}$

Active stress: $\underline{\underline{\sigma}}^a = \mathbb{C} \nabla_{\underline{x}} \underline{v} = 2\mu \text{sym}(\nabla_{\underline{x}} \underline{v})$

by frame indifference

$\mu = \text{abs viscosity}$

limit $\mu \rightarrow 0$ recovers ideal fluid

Navier Stokes Equations

Setting $p = p_0$ and $\underline{\underline{\sigma}} = -p \underline{\underline{I}} + 2\mu \underline{\underline{d}}$ linear

rep. theorem $\alpha_0(\underline{\underline{I}}_A) + \alpha_1(\underline{\underline{I}}_A) A + \cancel{HGT}$

$\alpha_0 = \text{tr}(\underline{\underline{\sigma}})$ $\alpha_1 = 2\mu$ by linearity

substitute into lin. mom. balance

$$\rho \cdot \underline{\dot{v}} = \nabla_x \cdot (-p \underline{\underline{I}} + 2\mu \underline{\underline{d}}) + \rho \cdot \underline{b}$$

$$\nabla_x \cdot \underline{\underline{\sigma}} = -\nabla_x p + \mu \nabla_x \cdot \nabla_x \underline{v} + \mu \nabla_x \cdot (\nabla_x \underline{v})^T$$

$$\nabla_x \cdot \nabla_x \underline{v} = v_{ijj} \underline{e}_i = \nabla_x^c \underline{v}$$

$$\nabla_x \cdot (\nabla_x \underline{v})^T = v_{jij} \underline{e}_i = v_{jji} \underline{e}_i = \nabla_x \cdot (\nabla_x \underline{v})$$

$$\Rightarrow \nabla_x \cdot \underline{\underline{\sigma}} = -\nabla_x p + \mu \nabla_x^c \underline{v}$$

Navier Stokes Equations

$$\rho \left[\frac{\partial \underline{v}}{\partial t} + (\nabla_x \underline{\sigma}) \underline{v} \right] = \mu \nabla_x^2 \underline{v} - \nabla_x p + \rho \underline{b}$$
$$\nabla_x \cdot \underline{v} = 0$$

Frame indifferent

already checked the constraint

\Rightarrow active stress

$$\underline{\underline{\sigma}}^a = 2\mu \underline{\underline{d}} = \mathbb{C} \nabla_x \underline{v}$$

Check left minor symmetry

$$(\mathbb{C} \nabla_x \underline{v})^T = (2\mu \underline{\underline{d}})^T = 2\mu \underline{\underline{d}}^T = 2\mu \underline{\underline{d}}^T = \mathbb{C} \nabla_x \underline{v}$$

Trace condition

$$\text{Tr}(\mathbb{C} \nabla_x \underline{v}) = 2\mu \text{tr}(\underline{\underline{d}}) = 0 \quad \text{if} \quad \text{tr}(\underline{\underline{d}}) = 0$$

Superposed rigid motion: $\underline{x}^* = \mathbb{Q}(t) \underline{x} + \underline{c}(t)$

$$\underline{\underline{\sigma}}^{a*} = \underline{\underline{\sigma}}^a(\underline{x}^*, t) \quad \underline{\underline{d}}^* = \underline{\underline{d}}(\underline{x}^*, t)$$

$$\text{show} \quad \underline{\underline{\sigma}}^{a*} = \mathbb{Q} \underline{\underline{\sigma}}^a \mathbb{Q}^T$$

$$\underline{\underline{\sigma}}^{a*} = 2\mu \underline{\underline{d}}^* = 2\mu \mathbb{Q} \underline{\underline{d}} \mathbb{Q}^T = \mathbb{Q} (2\mu \underline{\underline{d}}) \mathbb{Q}^T = \mathbb{Q} \underline{\underline{\sigma}}^a \mathbb{Q}^T$$

⇒ using result $\underline{\underline{d}}^* = \mathbb{Q} \underline{\underline{d}} \mathbb{Q}^T$ from Lecture 20.

⇒ Newtonian fluid model is frame indifferent.

Mechanical energy

$$\text{Dissipation: } \mathcal{D} = \underline{\underline{\sigma}} : \underline{\underline{d}} = (-p \underline{\underline{I}} + 2\mu \underline{\underline{d}}) : \underline{\underline{d}}$$

$$= -p \underbrace{\underline{\underline{I}} : \underline{\underline{d}}}_{\nabla_x \cdot \underline{v} = 0} + 2\mu \underline{\underline{d}} : \underline{\underline{d}}$$

Subst. into rel. Clausius-Duhem inequality

$$\rho \cdot \dot{\psi} \leq 2\mu \underline{d} : \underline{d} = 2\mu \underbrace{|\underline{d}|^2}_{>0}$$

\Rightarrow only if $\mu > 0$ energy dissipation during flow.

Kinetic energy during Fluid Motion

How (fast) is K dissipated in ideal & Newtonian flows.

First two results:

1) Integration by parts in fixed Ω with

$$\underline{v} = 0 \quad \partial\Omega$$

$$\int_{\Omega} (\nabla_x^2 \underline{v}) \cdot \underline{v} \, dV_x = - \int_{\Omega} (\nabla_x \underline{v}) : (\nabla_x \underline{v}) \, dV_x$$

consider

$$(v_{ij} v_i)_{,j} = v_{i,jj} v_i + v_{ij} v_{ij}$$

$$v_{i,jj} v_i = (v_{ij} v_i)_{,j} - v_{ij} v_{ij}$$

substitute

$$\begin{aligned} \int (\nabla_x^2 \underline{u}) \cdot \underline{u} dV_x &= \int_{\Omega} \nabla \cdot (\nabla_x^T \underline{u}) dV - \int (\nabla_x \underline{u}) : (\nabla_x \underline{u}) dV \\ &= \int_{\partial\Omega} \nabla_x^T \underline{u} \cdot \underline{n} dA - \int (\nabla_x \underline{u}) : (\nabla_x \underline{u}) dV \end{aligned}$$

0 on $\partial\Omega$

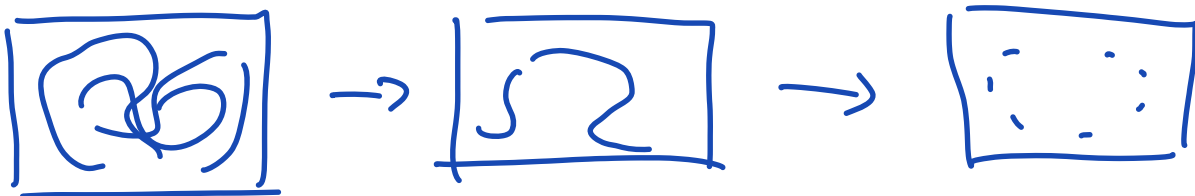
2) Poincaré inequality

$$\|\underline{u}\|_{\Omega} \leq \lambda \|\nabla_x \underline{u}\|_{\Omega} \quad \text{for } \underline{u} = 0 \text{ on } \partial\Omega, \lambda > 0$$

$$\int_{\Omega} |\underline{u}|^2 dV_x \leq \lambda \int_{\Omega} (\nabla_x \underline{u}) : (\nabla_x \underline{u}) dV_x$$

Units of λ $[L^2]$, constant that scales with area of domain Ω .

For fixed domain Ω with no-slip BC $\underline{u} = 0$ on $\partial\Omega$ and a conservative force field $\underline{b} = -\nabla_x \phi$ and kinetic energy $K(t) = \int_{\Omega} \frac{1}{2} \rho_0 |\underline{u}|^2 dV$ with $K(0) = K_0$



initial conditions with $K_0 > 0$, look at decay.

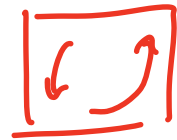
I) for Newtonian fluid

$$K(t) \leq K_0 e^{-2\mu t/\lambda\rho_0}$$

K dissipates exponentially

II) for ideal fluid

$$K(t) = K_0$$



From def of K

$$-\nabla p - \rho g \hat{z} = \frac{-\nabla(p - \rho g z)}{\rho}$$

$$\frac{d}{dt} K(t) = \frac{d}{dt} \int_{\Omega} \frac{1}{2} \rho_0 |\underline{v}|^2 dV_x = \int_{\Omega} \rho_0 \underline{\dot{v}} \cdot \underline{v} dV_x$$

from lin. mom. bal.: $\rho_0 \underline{\dot{v}} = \mu \nabla_x^2 \underline{v} - \nabla \psi$

$$\frac{d}{dt} K(t) = \int (\mu \nabla_x^2 \underline{v} - \nabla \psi) \cdot \underline{v} dV_x$$

show $\int \nabla \psi \cdot \underline{v} dV_x = 0$

$$\nabla_x \cdot (\psi \underline{v}) = \nabla_x \psi \cdot \underline{v} + (\nabla_x \cdot \underline{v}) \psi = \nabla_x \psi \cdot \underline{v}$$

subst and use div thm

$$\frac{d}{dt} K = \int_{\Omega} \mu \nabla_x^2 \underline{v} \cdot \underline{v} dV - \int_{\partial\Omega} \psi \underline{v} \cdot \underline{n} dA$$

by integration by parts

$$\frac{dK}{dt} = -\mu \int_{\Omega} (\nabla_x \underline{v}) : (\nabla_x \underline{v}) dV$$

if fluid is ideal $\mu \rightarrow 0$ $\frac{dk}{dt} = 0 \rightarrow k(t) = k_0$

for Newtonian fluid apply Poiseuille

$$\frac{d}{dt} k \leq -\frac{\mu}{\lambda} \int_{\Omega} |\underline{\sigma}|^2 dV_x = -\frac{2\mu}{\rho_0 \lambda} k(t)$$

so that

$$\frac{d}{dt} k \leq -\frac{2\mu}{\lambda \rho_0} k$$

with = an ode

for k -decay

by separation of parts

$$k \leq k_0 e^{-\frac{2\mu}{\lambda \rho_0} t}$$

λ = geometric factor

$\nu = \frac{\mu}{\rho_0}$ kinematic viscosity

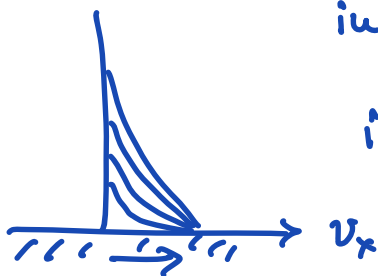
$$\mu = \left[\frac{M}{LT} \right] \quad \rho_0 = \left[\frac{M}{L^3} \right] \quad \nu = \frac{\mu}{\rho} = \left[\frac{L^2}{T} \right]$$

diffusion coefficient units

\Rightarrow momentum diffusivity

infinite fluid at rest

impulsively set to move and



erf-type solu

Scaling Navier-Stokes equ

$$\rho_0 \left(\frac{\partial \underline{v}}{\partial t} + (\nabla_x \underline{v}) \underline{v} \right) = \mu \nabla_x^2 \underline{v} - \nabla_x \pi$$

where $\pi = p + \rho g z$ "reduced pressure" ψ

dependent var.: \underline{v} , π

independent var.: \underline{x} , t

parameters: ρ , μ (ν)

+ geometry, BC, IC

Use parameters to render variable dimensionless

$$\underline{v}' = \frac{\underline{v}}{v_c} \quad \pi' = \frac{\pi}{\pi_c} \quad \underline{x}' = \frac{\underline{x}}{x_c} \quad t' = \frac{t}{t_c}$$

subst into lin. mom. bal.

$$\frac{\rho_0 v_c}{t_c} \frac{\partial \underline{v}'}{\partial t'} + \frac{\rho_0 v_c^2}{x_c} (\nabla_x' \underline{v}') \underline{v}' = \frac{\mu v_c}{x_c^2} \nabla_x'^2 \underline{v}' - \frac{\pi_c}{x_c} \nabla_x' \pi'$$

have to pick a term to scale to

\Rightarrow pick diff. mom. transport

divided by $\mu v_c / x_c^2$

$$\underbrace{\frac{x_c^2}{\nu t_c}}_{\Pi_1} \frac{\partial \underline{v}'}{\partial t'} + \underbrace{\frac{v_c x_c}{\nu}}_{\Pi_2} (\nabla_x' \underline{v}') \underline{v}' = \nabla_x'^2 \underline{v}' - \underbrace{\frac{\pi_c x_c}{\mu v_c}}_{\Pi_3} \nabla_x' \pi'$$

$$\Pi_3 = \frac{\pi_c x_c}{\mu v_c} = 1 \Rightarrow \pi_c = \frac{\mu v_c}{x_c}$$

How to pick t_c ? $t_c = t_A = \frac{x_c}{v_c}$ adv. timescale

$$\Pi_1 = \Pi_2 = \frac{v_c x_c}{\nu} = Re \quad \text{Reynolds number}$$

$$\text{Re} \left(\frac{\partial \underline{v}'}{\partial t'} + (\nabla'_x \underline{v}') \cdot \underline{v}' \right) = \nabla'_x{}^2 \underline{v}' - \nabla'_x \pi'$$

Dim. less Navier Stokes Equ.

Limit $Re \ll 1$

$$\nabla'_x{}^2 \underline{v}' = \nabla'_x \pi'$$

$$\nabla'_x \cdot \underline{v}' = 0$$

Re dimensionalize

$$\mu \nabla_x{}^2 \underline{v} = \nabla_x \pi$$

$$\nabla_x \cdot \underline{v} = 0$$

Stokes Equ

- linear & instantaneous