

Lecture 25: Newtonian Fluids

Logistics: - HW6 is graded

- HW8 please turn it in

Comment on HW6:

$$\nabla \underline{v} = \frac{\partial}{\partial x_j} \underline{e}_j \otimes v_i \underline{e}_i = \frac{\partial v_i}{\partial x_j} \underline{e}_i \otimes \underline{e}_j$$

$$\nabla \cdot \underline{v} = \frac{\partial}{\partial x_j} \underline{e}_j \cdot v_i \underline{e}_i = \frac{\partial v_i}{\partial x_j} \underbrace{\underline{e}_i \cdot \underline{e}_j}_{\delta_{ij}} = \frac{\partial v_i}{\partial x_i}$$

$$\nabla \cdot \underline{s} = s_{ij} \underline{e}_j$$

$$\nabla \cdot \underline{v} = \text{tr}(\nabla \underline{v})$$

⇒ can get you into trouble.

Today → Newtonian fluid

After Thanks giving → 1 week

⇒ Stokes fluids → glaciers

⇒ creep → non-linearity

Newtonian Fluids

A fluid is incompressible Newtonian if:

- 1) Reference mass density $\rho_0(\underline{x}) = \rho_0$
- 2) Fluid is incompressible $\nabla \cdot \underline{v} = 0$
- 3) Cauchy stress has form

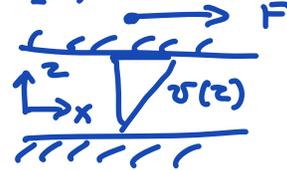
$$\underline{\underline{\sigma}} = \underline{\underline{\sigma}}^r + \underline{\underline{\sigma}}^a$$

$$\underline{\underline{\sigma}}^r = -p \underline{\underline{I}} \quad p = \text{pressure}$$

$$\underline{\underline{\sigma}}^a = 2\mu \text{sym}(\nabla \underline{v}) = \mu (\nabla \underline{v} + \nabla \underline{v}^T) \quad \text{Newtonian}$$

$$\text{Newton: } \tau \sim \frac{d\sigma}{dz}$$

$$\tau = \mu \frac{d\sigma}{dz}$$



\Rightarrow both $\underline{\underline{\sigma}}^r$ and $\underline{\underline{\sigma}}^a$ are objective

\Rightarrow $\underline{\underline{\sigma}} = -p \underline{\underline{I}} + \mu (\nabla \underline{v} + \nabla \underline{v}^T)$ is also objective

limit of $\mu \rightarrow 0$ reduces to ideal fluid.

Navier - Stokes Equations

lin. mom. balance: $\rho \dot{\underline{v}} = \nabla \cdot \underline{\underline{\underline{\sigma}}} + \rho \underline{b}$

subst: $\rho = \rho_0$ $\underline{\underline{\underline{\sigma}}} = -p \underline{\underline{\underline{I}}} + \mu (\nabla \underline{v} + \nabla \underline{v}^T)$

$$\rho_0 \dot{\underline{v}} = \nabla \cdot (-p \underline{\underline{\underline{I}}} + 2\mu \text{sym}(\nabla \underline{v})) + \rho_0 \underline{b}$$

mat. deriv: $\dot{\underline{v}} = \frac{\partial \underline{v}}{\partial t} + (\nabla \underline{v}) \underline{v}$

assume $\mu = \text{const.}$

$$\nabla \cdot \underline{\underline{\underline{\sigma}}} = -\nabla p + \mu \nabla \cdot \nabla \underline{v} + \mu \nabla \cdot \nabla \underline{v}^T$$

$$\nabla \cdot \nabla \underline{v} = \nabla^2 \underline{v}$$

$$\nabla \cdot (\nabla \underline{v})^T = v_{j,i} e_j = v_{j,i} e_i = \nabla (\nabla \cdot \underline{v})$$

$$\Rightarrow \nabla \cdot \underline{\underline{\underline{\sigma}}} = -\nabla p + \mu \nabla^2 \underline{v}$$

so that:

last lecture ideal $\mu = 0$

$$\rho_0 \left[\frac{\partial \underline{v}}{\partial t} + (\nabla \underline{v}) \underline{v} \right] = \mu \nabla^2 \underline{v} - \nabla p + \rho_0 \underline{b}$$

$\nabla \cdot \underline{\underline{\underline{\sigma}}} = 0$

Navier Stokes equations

$$(\nabla \underline{v}) \underline{v} = (\underline{v} \cdot \nabla) \underline{v}$$

Energy dissipation

Stress power of Newtonian fluid: $d = \text{sym}(\nabla \underline{v})$

$$\begin{aligned}\underline{\underline{\sigma}} : \underline{\underline{d}} &= (-p \underline{\underline{I}} + 2\mu \underline{\underline{d}}) : \underline{\underline{d}} \\ &= -p \underbrace{\underline{\underline{I}} : \underline{\underline{d}}}_{\nabla \cdot \underline{v} = 0} + 2\mu \underline{\underline{d}} : \underline{\underline{d}}\end{aligned}$$

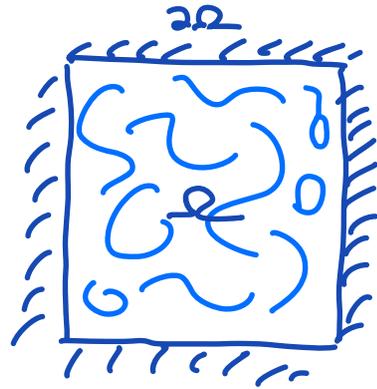
$$\underline{\underline{\sigma}} : \underline{\underline{d}} = 2\mu \underbrace{\underline{\underline{d}} : \underline{\underline{d}}}_{> 0}$$

if $\mu > 0$ then energy is dissipated by the flow

Kinetic Energy in Fluid Motion

Dissipation of kinetic energy
in ideal & Newtonian fluids:

Show how energy decays in
closed domain with initial flow.



First some results:

By definition of kinetic energy

$$\begin{aligned} \frac{d}{dt} K(t) &= \frac{d}{dt} \int_{\Omega} \frac{1}{2} \rho_0 |\underline{v}|^2 d\Omega = \int_{\Omega} \frac{1}{2} \rho_0 \frac{d}{dt} |\underline{v}|^2 dV \\ &= \int_{\Omega} \rho_0 \underline{\dot{v}} \cdot \underline{v} dV \end{aligned}$$

from N-S: $\underline{\rho \dot{v}} = \mu \nabla^2 \underline{v} - \rho \nabla \psi$ $\underline{b} = -\nabla \psi$

$$\frac{d}{dt} K(t) = \int_{\Omega} (\mu \nabla^2 \underline{v} - \rho \nabla \psi) \cdot \underline{v} dV$$

$$= \int_{\Omega} (\mu \nabla^2 \underline{v}) \cdot \underline{v} dV - \int_{\Omega} \rho \nabla \psi \cdot \underline{v} dV$$

$$\nabla \cdot (\psi \underline{v}) = \nabla \psi \cdot \underline{v} + (\nabla \cdot \underline{v}) \psi$$

$$\nabla \cdot (\psi \underline{v}) = \nabla \psi \cdot \underline{v}$$

$$\int_{\Omega} \nabla \psi \cdot \underline{v} dV = \int_{\Omega} \nabla \cdot (\psi \underline{v}) dV = \oint_{\partial \Omega} \psi \underline{v} \cdot \underline{n} dA$$

$$\Rightarrow \frac{d}{dt} K(t) = \mu \int_{\Omega} \nabla^2 \underline{v} \cdot \underline{v} dV = -\mu \int_{\Omega} \underbrace{\nabla \underline{v} : \nabla \underline{v}}_{\leq \frac{1}{\lambda} |\underline{v}|^2} dV$$

$$\frac{d}{dt} K(t) \leq -\frac{\mu}{\lambda} \int_{\Omega} |\underline{v}|^2 dV = -\frac{2\mu}{\lambda \rho_0} K(t)$$

ODE for K

$$\frac{d}{dt} K(t) = -\frac{2\mu}{\lambda \rho_0} K(t)$$

λ = depends on domain

Solve by separation of variables

$$\frac{dK}{K} = -\underbrace{\frac{2\mu}{\lambda \rho_0}}_{\alpha} dt = -\alpha dt$$

$$\ln(K) = -\alpha t + c_0$$

$$K = \zeta e^{-\alpha t}$$

Initial condition: $K(0) = c = K_0$

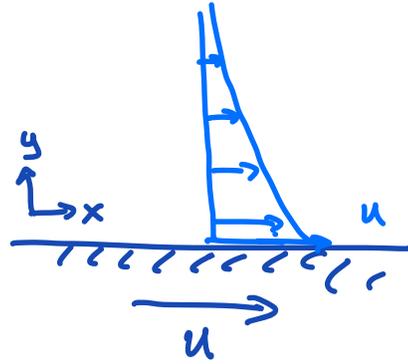
$$\Rightarrow K(t) = K_0 e^{-\frac{2\mu}{\lambda \rho_0} t}$$

In absence of fluid motion on boundary
the kinetic energy decays exponentially

Rate of decay: $\nu = \frac{\mu}{\rho_0}$ kinematic viscosity
 $\nu \left[\frac{L^2}{T} \right] \Rightarrow$ diffusion $\mu =$ dynamic viscosity

Rayleigh's first problem

- Semi-infinite half space
- Fluid is initially stationary
- Impulsively started plate with velocity u



$$\rho_0 \frac{\partial \underline{v}}{\partial t} + (\nabla \underline{v}) \underline{v} = \mu \nabla^2 \underline{v} - \nabla p + \rho g$$

reduced pressure:

$$-\nabla p + \rho g = -\nabla p - \rho g \hat{y} = -\nabla \underbrace{(p + \rho g y)}_{\pi} = -\nabla \pi$$

$$\pi = p + \rho g z = \text{reduced pressure}$$

$(\nabla \underline{v}) \underline{v}$ is quadratic in \underline{v}
 if \underline{v} small $(\nabla \underline{v}) \underline{v} \rightarrow$ is negligible.

$$\Rightarrow \rho \frac{\partial \underline{v}}{\partial t} = \mu \nabla^2 \underline{v} - \nabla \pi$$

Stokes

is linear
 $\underline{v} = \begin{pmatrix} u \\ w \end{pmatrix} \begin{matrix} x \\ y \end{matrix}$

Simplify eqns:

because domain is infinite but $|\pi| < \infty = \frac{\partial \pi}{\partial x} = 0$

flow is horizontal: $\underline{v} = \begin{pmatrix} u \\ 0 \end{pmatrix}$ $w = 0$

from continuity: $\nabla \cdot \underline{v} = \frac{\partial u}{\partial x} + \frac{\partial w}{\partial y} = 0$

$\Rightarrow \underline{u} = u(y)$

$\nabla^2 \underline{u} = v_{i,jj} \underline{e}_i \quad i,j \in \{1,2\}$

$v_1 = u \quad v_2 = w$

$\nabla^2 \underline{u} = \begin{pmatrix} v_{1,11} & v_{1,22} \\ v_{2,11} & v_{2,22} \end{pmatrix} = \begin{pmatrix} \cancel{u_{xx}} & u_{xy} \\ \cancel{w_{xx}} & \cancel{w_{xy}} \end{pmatrix} = \begin{pmatrix} u_{yy} \\ 0 \end{pmatrix}$

substitute

x-mom: $\rho \frac{\partial u}{\partial t} - \mu \frac{\partial^2 u}{\partial x^2} = 0$

y-mom: $0 = -\frac{\partial \pi}{\partial y}$

$\Rightarrow \boxed{\frac{\partial u}{\partial t} = \nu \frac{\partial^2 u}{\partial x^2}} \quad u = u(y)$

BC: $u(t, x=0) = u$

IC: $u(t=0, x) = 0$

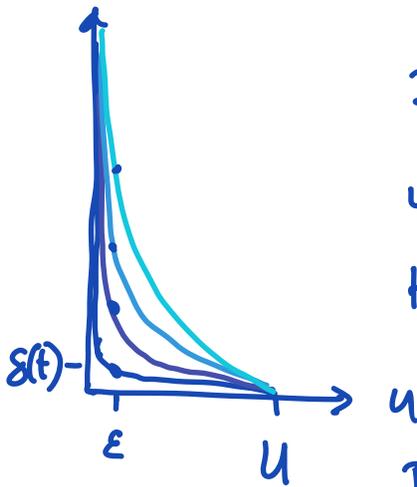
\Rightarrow diffusion equation

Heat equation: $\cancel{\rho c_p} \frac{\partial T}{\partial t} = \frac{k}{\cancel{\rho c_p}} \nabla^2 T = \underbrace{\frac{k}{\rho c_p}}_{\alpha} \frac{\partial^2 T}{\partial x^2}$

Classic analytic solution for diffusion:

$$\Rightarrow u(y,t) = U \left(1 - \operatorname{erf} \left(\frac{y}{\sqrt{4\nu t}} \right) \right)$$

\Rightarrow see notes for self-similar ansatz.



Diffusive boundary layer
where momentum is added
to fluid from moving boundary

Boundary layer thickness: 10^{-6}

$$\delta \sim 2\sqrt{\nu t}$$

$$\frac{\mu}{\rho} = \frac{10^{-3}}{10^3} \text{ Pa}\cdot\text{s}$$

$\nu = \frac{\mu}{\rho_0}$ is momentum diffusivity

