

# Momentum diffusion

Remember where terms come from

lin. mom. bal.:  $\rho \dot{\underline{v}} = \underline{\nabla} \cdot \underline{\underline{\sigma}} + \rho \underline{g}$

Newtonian

$$\underline{\underline{\sigma}} = -p \underline{\underline{I}} + \mu (\underline{\nabla} \underline{v} + \underline{\nabla} \underline{v}^T)$$

Navier-Stokes:  $\frac{\partial \underline{v}}{\partial t} + \underline{v} \cdot \underline{\nabla} \underline{v} = \underline{\nu} \nabla^2 \underline{v} - \frac{1}{\rho} \underline{\nabla} \pi$

kinematic viscosity:  $\nu = \frac{\mu}{\rho} \quad \left[ \frac{\text{m}^2}{\text{s}} \right]$

$$\mu = \text{Pa s} = \frac{\text{kg}}{\text{m s}} \quad \rho = \frac{\text{kg}}{\text{m}^3}$$

$\Rightarrow$  units of diffusivity

Today we'll show that  $\nu$  characterizes momentum diffusion!

Scaled N-S equations:

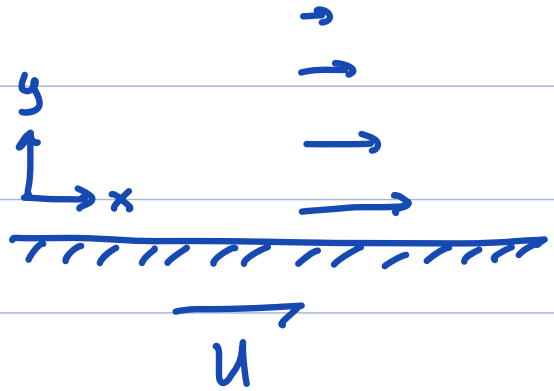
$$\frac{\partial \underline{v}}{\partial t} + \text{Re} \underline{v} \cdot \underline{\nabla} \underline{v} = \nabla^2 \underline{v} - \underline{\nabla} \pi$$

$$\text{Re} = \frac{v_c x_c}{\nu} \quad \text{Reynolds number}$$

Today  $\text{Re} \ll 1$

# Rayleigh's problem

- Semi-infinite half-space
- Stationary fluid
- Impulsively started plate with velocity  $U$ .



$$v_c = U \rightarrow Re = \frac{U x_c \rho_0}{\mu} \ll 1 \Rightarrow U \ll \frac{\mu}{x_c \rho_0}$$

But what is  $x_c$ ? Not obvious

Redimensionalize assuming  $Re \ll 1$

$$\frac{\partial \underline{v}}{\partial t} - \nu \nabla^2 \underline{v} = -\nabla \pi \quad \& \quad \nabla \cdot \underline{v} = 0 \quad \underline{v} = \begin{pmatrix} u \\ w \end{pmatrix}$$

Simplify the equations:

Domain is infinite in  $x$  but  $|\pi| < \infty \Rightarrow \frac{\partial \pi}{\partial x} = 0$

Flow is horizontal:  $\underline{v} = \begin{pmatrix} u \\ w \end{pmatrix} \Rightarrow w = 0$

From continuity:  $\frac{\partial u}{\partial x} + \frac{\partial w}{\partial y} = 0 \Rightarrow \frac{\partial u}{\partial x} = 0 \Rightarrow u = u(y)$

$$\nabla^2 \underline{v} = v_{i,jj} \underline{e}_i \quad i, j \in \{1, 2\}$$

$$= \begin{pmatrix} v_{1,11} & v_{1,22} \\ v_{2,11} & v_{2,22} \end{pmatrix} = \begin{pmatrix} \cancel{u_{xx}} & u_{yy} \\ \cancel{w_{xx}} & \cancel{w_{yy}} \end{pmatrix} = \begin{pmatrix} u_{yy} \\ 0 \end{pmatrix}$$

Substituting we have

$$x\text{-mom.: } \frac{\partial u}{\partial t} - \nu \frac{\partial^2 u}{\partial x^2} = 0$$

$$y\text{-mom.: } 0 = -\frac{\partial \pi}{\partial y} \Rightarrow \nabla \pi = \underline{0}$$

$$\Rightarrow \boxed{\frac{\partial u}{\partial t} = \nu \frac{\partial^2 u}{\partial x^2}} \quad \text{with } u(0, y) = 0 \quad u(t, 0) = U$$

This is identical to heating a semi-infinite rod from the end.

Problem has self-similar solution in

$$\eta = \frac{y}{\sqrt{4\nu t}} \quad \text{and} \quad u(y, t) = U f(\eta)$$

where  $\sqrt{4\nu t}$  takes role of char. length that depends on  $t$ .

$$\text{derivatives: } \frac{\partial \eta}{\partial t} = -\frac{1}{2} \frac{\eta}{t} \quad \frac{\partial \eta}{\partial y} = \frac{1}{\sqrt{4\nu t}}$$

The derivatives of  $u$  transform as:

$$\frac{\partial u}{\partial t} = U \frac{df}{d\eta} \frac{\partial \eta}{\partial t} = -\frac{U}{2} \frac{\eta}{t} \quad \text{and} \quad \frac{\partial^2 u}{\partial x^2} = U \frac{d^2 f}{d\eta^2} \left( \frac{\partial \eta}{\partial x} \right)^2 = \frac{U}{4\nu t} \frac{d^2 f}{d\eta^2}$$

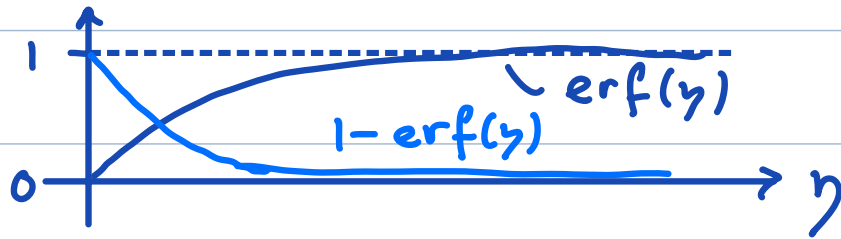
substituting into PDE:

$$\frac{d^2 f}{d\eta^2} + 2\eta \frac{df}{d\eta} = 0 \quad \text{with } f(\eta=0) = 1$$

Reduce PDE in  $y$  and  $t$  to ODE in  $\eta$

Solution:  $f(\eta) = 1 - \text{erf}(\eta)$  (Gauss)

where  $\text{erf}(\eta) = \frac{2}{\sqrt{\pi}} \int_0^\eta e^{-\xi^2} d\xi$  error function



Resubstituting for  $f = \frac{u}{U}$  and  $\eta = \frac{y}{\sqrt{4\nu t}}$

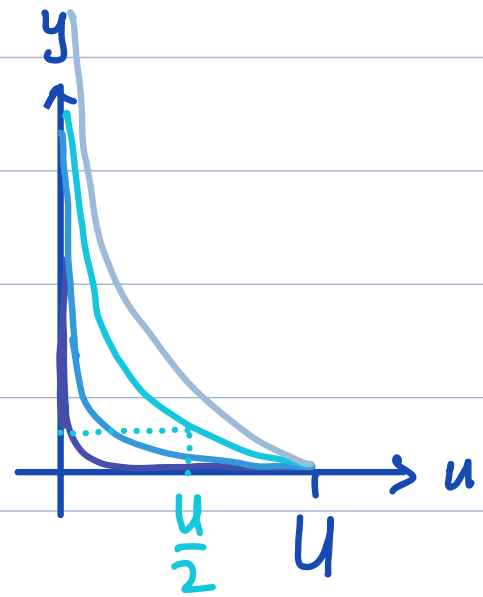
$$u(y,t) = U \left( 1 - \text{erf} \left( \frac{y}{\sqrt{4\nu t}} \right) \right)$$

Diffusive boundary layer

where momentum added

by boundary penetrates  
into the quiescent fluid.

$2\sqrt{\nu t}$



$\nu = \frac{\mu}{\rho_0}$  is Diffusion coefficient.

$\Rightarrow$  shear stress causes momentum diffusion

lin. mom. bal.:  $\rho \dot{\underline{v}} = \nabla \cdot \underline{\underline{\sigma}} + \rho \underline{g}$

rewrite in conservative form:

$$\frac{\partial}{\partial t}(\rho \underline{v}) + \nabla \cdot [\underbrace{\rho \underline{v} \otimes \underline{v}}_{\text{adv. flux}} - \underbrace{\underline{\underline{\sigma}}}_{\text{diffusive flux}}] = \rho \underline{g}$$

Energy dissipation in viscous boundary layer

stress power:  $\phi = \underline{\underline{\sigma}} : \underline{\underline{d}} \quad \underline{\underline{\sigma}} = -p \underline{\underline{I}} + 2\mu \underline{\underline{d}}$

$$= -p \underline{\underline{I}} : \underline{\underline{d}} + 2\mu \underline{\underline{d}} : \underline{\underline{d}}$$

$$\underline{\underline{I}} : \underline{\underline{d}} = \delta_{ij} \frac{1}{2} (v_{i,j} + v_{j,i}) = v_{i,i} = \nabla \cdot \underline{v} = 0 \text{ incomp.}$$

$\Rightarrow \boxed{\phi = 2\mu \underline{\underline{d}} : \underline{\underline{d}}}$  stress power in incompressible fluid

Example:  $u(y,t) = U \left[ 1 - \operatorname{erf}\left(\frac{y}{\sqrt{4\nu t}}\right) \right]$

$$2D: \nabla \underline{v} = \begin{bmatrix} u_{,x} & u_{,y} \\ w_{,x} & w_{,y} \end{bmatrix} = \begin{bmatrix} 0 & u_{,y} \\ 0 & 0 \end{bmatrix}$$

$$\underline{\underline{d}} = \frac{1}{2} \begin{bmatrix} 0 & u_{,y} \\ u_{,y} & 0 \end{bmatrix}$$

stress power:  $\phi = 2\mu \underline{d} : \underline{d} = 2\mu d_{ij} d_{ij}$   
 $= 2\mu \left[ \frac{1}{4} (u_{,y})^2 + \frac{1}{4} (u_{,y})^2 \right]$

$$\phi = \mu (u_{,y})^2$$

$$\frac{\partial u}{\partial y} = -u \frac{d}{dy} \operatorname{erf}\left(\frac{y}{\sqrt{4\nu t}}\right) = -u \frac{d}{dy} \operatorname{erf}(\eta) \frac{dy}{dy}$$

$$\operatorname{erf}(\eta) = \frac{2}{\sqrt{\pi}} \int_0^\eta e^{-\xi^2} d\xi \Rightarrow \frac{d}{d\eta} \operatorname{erf}(\eta) = \frac{2}{\sqrt{\pi}} e^{-\eta^2}$$

$$\frac{d\eta}{dy} = \frac{1}{\sqrt{4\nu t}}$$

$$\Rightarrow \frac{\partial u}{\partial t} = -\frac{u}{\sqrt{\pi\nu t}} e^{-\frac{y^2}{4\nu t}}$$

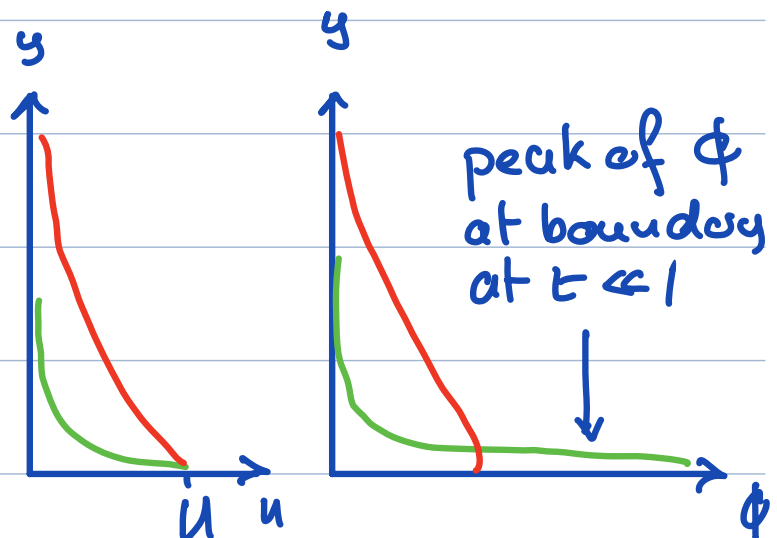
Energy dissipation:

$$\phi = \mu \left(\frac{\partial u}{\partial y}\right)^2 = \frac{\mu u^2}{\pi \nu t} e^{-\frac{y^2}{4\nu t}} = \frac{\rho u^2}{\pi t} e^{-\frac{y^2}{4\nu t}}$$

$\uparrow$   
 $\mu/\rho$

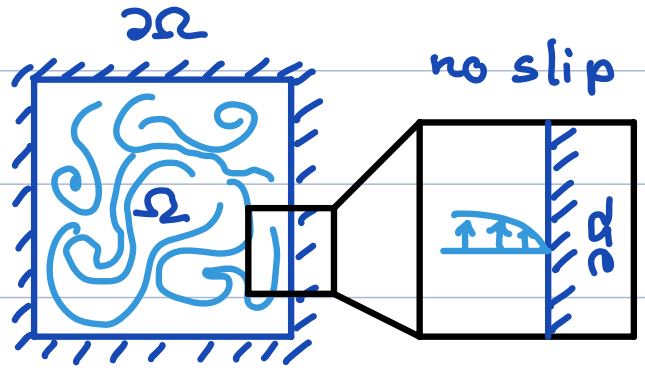
$$\phi(y,t) = \frac{\rho u^2}{\pi t} e^{-\frac{\rho y^2}{4\mu t}}$$

Gaussian



# Kinetic Energy of Fluid Motion

Dissipation of kinetic energy in a closed domain with no-slip boundaries.



$\Rightarrow$  Energy is lost by boundary

Change in kinetic energy

$$\frac{d}{dt} K(t) = \int_{\Omega} \frac{1}{2} \rho \frac{d}{dt} |\underline{v}|^2 dV = \int_{\Omega} \rho \underline{\dot{v}} \cdot \underline{v} dV$$

from Navier-Stokes Eqs:  $\rho_0 \underline{\dot{v}} = \mu \nabla_x^2 \underline{v} - \nabla \pi$

$$\frac{d}{dt} K(t) = \int_{\Omega} (\mu \nabla^2 \underline{v} - \nabla \pi) \cdot \underline{v} dV$$

$$\Rightarrow \frac{dK}{dt} = \mu \int_{\Omega} \nabla^2 \underline{v} \cdot \underline{v} dV - \mu \int_{\Omega} \nabla \pi \cdot \underline{v} dV$$

$\Rightarrow$  show second term is zero

$$\nabla \cdot (\pi \underline{v}) = \underline{v} \cdot \nabla \pi + \pi \nabla \cdot \underline{v}$$

$$\int_{\Omega} \nabla \pi \cdot \underline{v} \, dV = \int_{\Omega} \nabla \cdot (\pi \underline{v}) \, dV = \int_{\partial \Omega} (\pi \underline{v}) \cdot \hat{n} \, dA$$

$\underline{v} = 0$  on  $\partial \Omega$

$$\Rightarrow \frac{dK}{dt} = \mu \int_{\Omega} \nabla^2 \underline{v} \cdot \underline{v} \, dV = ?$$

$$\begin{aligned} \nabla^2 \underline{v} \cdot \underline{v} &= v_{i,jj} \cdot v_i = (v_{i,j} v_i)_{,j} - v_{i,j} v_{i,j} \\ &= \nabla \cdot (\nabla^T \underline{v} \underline{v}) - \nabla \underline{v} : \nabla \underline{v} \end{aligned}$$

$$\frac{dK}{dt} = \mu \int_{\Omega} \nabla \cdot (\nabla^T \underline{v} \underline{v}) \, dV - \mu \int_{\Omega} \nabla \underline{v} : \nabla \underline{v} \, dV$$

$$= \mu \int_{\partial \Omega} (\nabla^T \underline{v} \underline{v}) \cdot \hat{n} \, dA - \mu \int_{\Omega} \nabla \underline{v} : \nabla \underline{v} \, dV$$

$$\frac{dK}{dt} = -\mu \int_{\Omega} \nabla \underline{v} : \nabla \underline{v} \, dV$$

Poincaré Inequality

$$\|\underline{v}\|_{\Omega} \leq \lambda \|\nabla \underline{v}\|_{\Omega} \quad \text{for } \underline{v} = 0 \quad \partial \Omega \quad \lambda > 0$$

using standard inner product

$$\int_{\Omega} |\underline{v}|^2 \, dV \leq \lambda \int_{\Omega} \nabla \underline{v} : \nabla \underline{v} \, dV$$



Notice  $\lambda$  has units of  $L^2$  and scales with area of  $\Omega$ .

$$\frac{dk}{dt} \leq -\mu \lambda \int_{\Omega} |\underline{v}|^2 dV = -\underbrace{\frac{\mu \lambda}{\rho_0} \int_{\Omega} \rho |\underline{v}|^2 dV}_K$$

$$\Rightarrow \boxed{\frac{dk}{dt} \leq -\frac{\mu \lambda}{\rho_0} K}$$

Solve by separation of parts

$$\frac{dk}{K} \leq -\frac{\mu \lambda}{\rho_0 \lambda} dt = -\alpha dt$$

$$\ln k \leq -\alpha t + c_0$$

$$k \leq c_1 e^{-\alpha t}$$

Initial condition  $k(0) \leq c_1 = k_0$

$$\boxed{K(t) \leq k_0 e^{-\frac{\nu}{\lambda} t}}$$

$\nu = \frac{\mu}{\rho}$  mom. diffusivity

$\lambda =$  geometric factor