

## Lecture 2: Balance laws

Jan 21, 2021

Logistics: - Office hours

Tu 12-2 pm

Mo 9-10 am

same Zoom link

Fr 4:30-6 pm

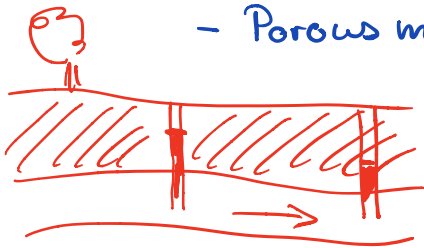
- HW 1 posted on Matlab Grades due Feb 4<sup>th</sup>

Last time: - Course logistics

- Course project: ground water flow

into impact craters on Mars

- Porous media: - "Darcy scale" vs "Pore scale"



- saturated vs. unsaturated

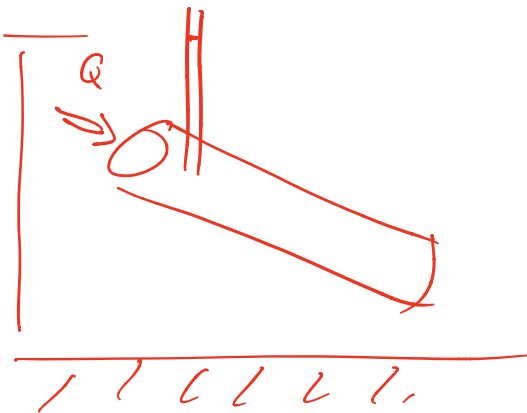
- volume fractions, saturations

- Darcy's law:  $q = -K \nabla h$

$q = \text{vol. flux} \left[ \frac{L^3}{L^2 T} \right]$  (specific discharge)

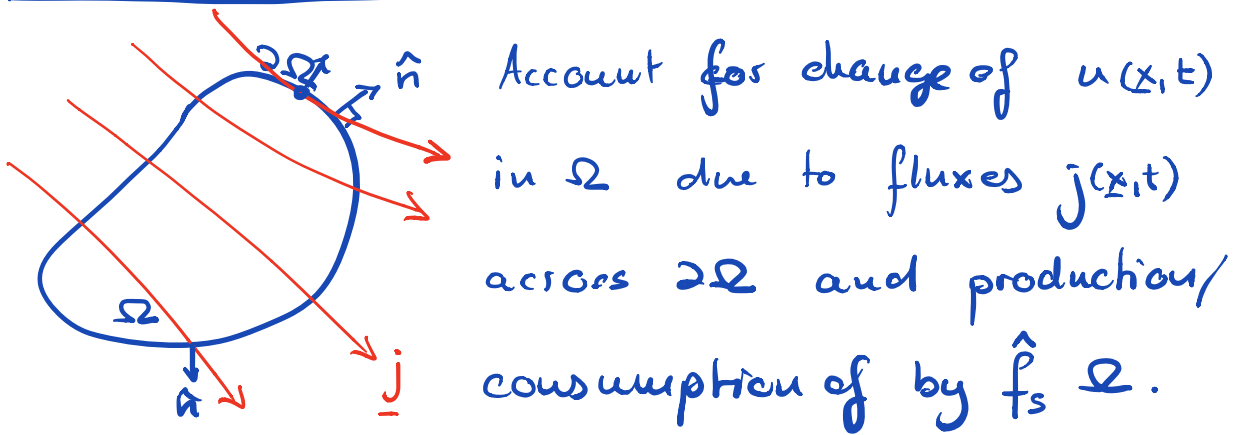
$h = \text{hydraulic head} [L]$

$K = \text{hydraulic conductivity}$



- Today:
- Derivation of general balance law
  - Fluid mass balance
  - Incompressible flow
- ⇒ Governing eqn for steady saturated flow

## General balance law



Units of basic quantities:

- $u$  is a density  $\left[ \frac{\#}{L^3} \right]$
- $\underline{j}$  is a flux  $\left[ \frac{\#}{L^2 T} \right]$
- $\underline{\hat{f}}_s$  is a vol. rate  $\left[ \frac{\#}{L^3 T} \right]$

General Macroscopic balance:

$$\frac{d}{dt} U = J + F$$

1)  $U$  is amount of  $u(\underline{x}, t)$  in  $\Omega$ :  $U(t) = \int_{\Omega} \underline{u} \, dV$   
#  $\frac{\#}{L^3} L^3$

2)  $J$  is rate of transport of  $\underline{u}$  across  $\partial\Omega$ .

$$J(t) = - \oint_{\partial\Omega} \underline{j} \cdot \hat{n} \, dA$$

#  $\frac{\#}{L^2 T} L^2$

3)  $F$  is rate of prod./cons. of  $\underline{u}$  in  $\Omega$ :

$$F(t) = \int_{\Omega} \hat{f}_s \, dV$$

#  $\frac{\#}{L^3 T} L^3$

$$\frac{dU}{dt} = J + F$$

#  $\frac{\#}{T}$     #  $\frac{\#}{T}$     #  $\frac{\#}{T}$     ✓

To obtain microscopic balance law

⇒ substitute def. of  $U, J, F$

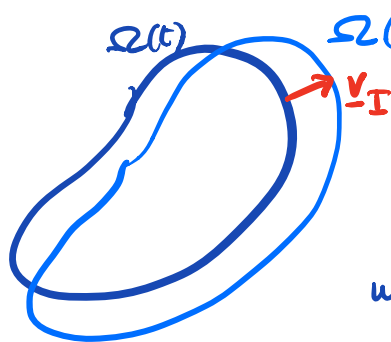
$$\frac{d}{dt} \int_{\Omega} u \, dV = - \oint_{\partial\Omega} \underline{j} \cdot \hat{n} \, dA + \int_{\Omega} \hat{f}_s \, dV$$

Integral balance law

To obtain a local PDE we need to:

- 1) Exchange derivative integral
- 2) Transform surface integral to vol. int.

1) Reynolds transport theorem



If  $\Omega$  is moving  $\underline{v}_I(\underline{x})$

$$\frac{d}{dt} \int_{\Omega(t)} \underline{u}(\underline{x}, t) \, dV = \int_{\Omega} \frac{\partial \underline{u}}{\partial t} \, dV + \oint_{\partial\Omega} \underline{u} (\underline{v}_I \cdot \hat{n}) \, dA$$

↑ material                      ↑ partial

We consider the Eulerian limit  $\underline{v}_I = 0$

$$\Rightarrow \frac{d}{dt} \int_{\Omega} u \, dV = \int \frac{du}{dt} \, dV \quad \checkmark$$

2) Divergence thm:  $\oint_{\partial\Omega} \underline{j} \cdot \underline{n} \, dA = \int_{\Omega} \nabla \cdot \underline{j} \, dV$

substitute:  $\int_{\Omega} \left( \frac{\partial u}{\partial t} + \nabla \cdot \underline{j} - \hat{f}_s \right) dV = 0$

$\underbrace{\hspace{10em}}_{g(\underline{x}, t)}$

Localization: This holds for any  $\Omega$

$$\int_{\Omega} g(\underline{x}, t) \, dV = 0$$

The integrand  $g$  must be zero everywhere.

Local form of general balance law

$$\frac{\partial u}{\partial t} + \nabla \cdot \underline{j} = \hat{f}_s$$

$\frac{\#}{L^3 T} \quad \downarrow \quad \frac{\#}{L^2 T} \quad = \quad \frac{\#}{L^3 T}$

$u = \text{unknown} \quad [\# / L^3]$

$\underline{j} = \text{flux} \quad [\# / (L^2 T)]$

$\hat{f}_s = \text{source/sink} \quad [\# / (L^3 T)]$

# Fluid Mass Balance in a saturated p.m.

Start from general balance and define

$$u, \underline{j} \text{ and } \underline{f}_s$$

1) unknown  $u$  to be balanced

$$\underline{u} \equiv \underline{\phi} \rho \quad \rho = \text{mass density} \left[ \frac{M}{L^3} \right]$$

$$\phi = \text{porosity} [1]$$

$\Rightarrow u$  is the fluid mass per unit volume of porous medium

2) Define the mass flux of fluid

$$\underline{j}(u) = \underline{j}(\phi \rho) = \rho \phi \underline{v} = \rho \underline{q}$$



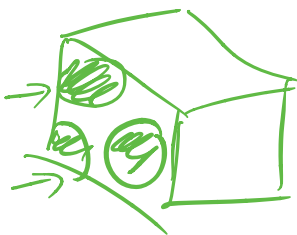
$\underline{v}$  = ave. interstitial fluid velocity  $\left[ \frac{L}{T} \right]$

$$\underline{q} = \phi \underline{v}$$

$\frac{L}{T} \quad | \quad \frac{L}{T}$

vol. flux given by

Darcy's law



3) Source term:  $\hat{f}_s = \rho f_s$

$$\frac{M}{L^3 T} \quad \frac{M}{L^3} \frac{L^3}{L^3 T}$$

$f_s \left[ \frac{1}{T} \right]$

Substitute into ~~the~~ general balance

$$\frac{\partial}{\partial t}(\phi \rho) + \nabla \cdot (\rho q) = \rho f_s$$

Fluid mass balance  
in sat. p.m.

To solve single PDE for single unknown we need constitutive laws.

1) Darcy's law:  $q = -\underline{k} \nabla h$

2) Equation of state:  $\rho = \rho(p) = \rho(h)$

$$h \sim p \quad \left( h = \frac{p - p_0}{\rho g} \right)$$

$$\frac{\partial}{\partial t}(\phi(x) \rho(h)) - \nabla \cdot (\rho(h) \underline{k} \nabla h) = \rho(h) f_s$$

$\Rightarrow$  can be solved for  $h(x, t)$

## Incompressible flow

- pressure variations during GW flow small  $\Rightarrow \rho = \rho_0 = \text{const.}$
- porosity & hydr. cond. are functions of space but not time

$$\frac{\partial}{\partial t} (\cancel{\rho(x)} \rho_0) + \nabla \cdot (\cancel{\rho_0} \mathbf{q}) = \cancel{\rho_0} f_s$$

$\Rightarrow$  continuity equation

$$\nabla \cdot \mathbf{q} = f_s$$

Substituting Darcy's law  $\mathbf{q} = -K \nabla h$

$$\Rightarrow -\nabla \cdot (\underline{K} \nabla h) = f_s$$

Incompressible  
saturated GW flow  
(Poisson Equ)

no time dependence  $\rightarrow$  steady



## Boundary value problem (BVP)

A well posed problem requires boundary cond.

$$\text{PDE: } \nabla \cdot \mathbf{q} = f_s$$
$$\mathbf{q} = -k \nabla h$$

BC: a) Dirichlet BC

prescribe value of  
unknown on the boundary

$$h(\underline{x}) = h_B(\underline{x}) \quad \underline{x} \in \partial\Omega_D$$

Example: Lake provides const head



b) Neuman BC

prescribes the value of flux on the

boundary  $\mathbf{q} \cdot \hat{\mathbf{n}} = -q_B \quad \underline{x} \in \partial\Omega_N$

$q_B > 0$  is an inflow

Example: Rain fall

