

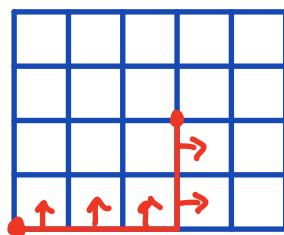
Lecture 24: Variable viscosity Stokes flow

Logistics: - HW 8 is due

- HW 9 will be posted (Lid driven cavity)

Last time: - Streamfunction

- $\Psi = - \int v_y dx + \int v_x dy$
- Ψ (is single valued) if $\nabla \cdot \underline{v} = 0$
- Numerical implementation



Ψ is on cell corners
simply sum up fluxes
along faces

Today: - Variable viscosity

Example of Couette flow
with T-gradient.

Temperature dependent viscosity

- most common source of non-linearity is variation of viscosity with Temperature
- ice rheology is complex because it depends on the microscopic deformation mechanism
- We consider "diffusion creep" which results in Newtonian rheology

$$\mu = \frac{RT d^2}{42 V_m D_{o,v}} \exp\left(\frac{E_A}{RT}\right)$$

Parameters: d = grain diameter $\approx 1 \text{ mm}$

T = temp.

V_m = molar volume $1.97 \cdot 10^{-5} \frac{\text{m}^3}{\text{mol}}$

$D_{o,v}$ = vol. diff. const $9.1 \cdot 10^{-4} \frac{\text{m}^2}{\text{s}}$

E_A = activation energy $60 \frac{\text{kJ}}{\text{mol}}$

R = univ. gas const. $8.3 \dots \frac{\text{J}}{\text{K mol}}$

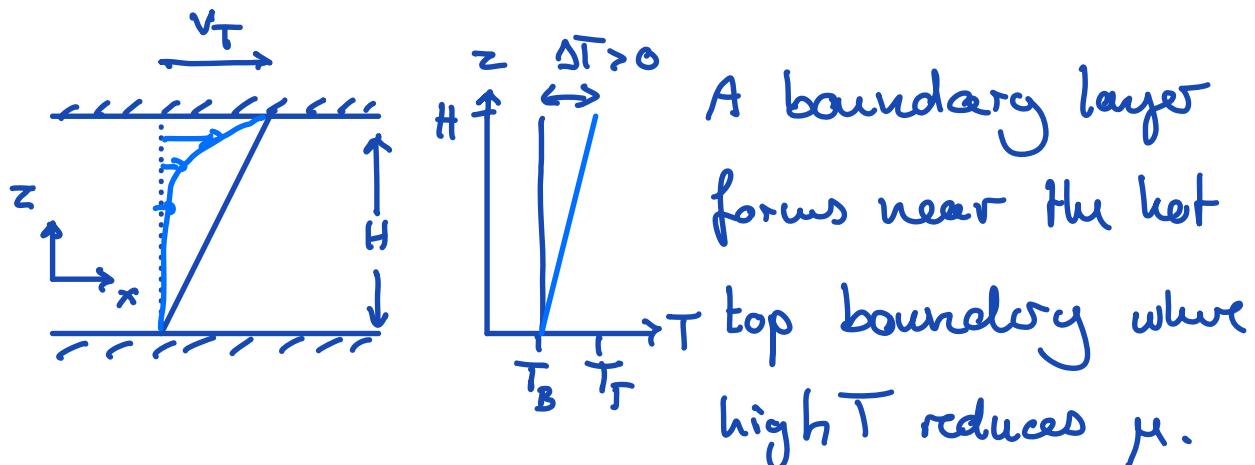
Newtonian: $\mu \neq \mu(v)$

but μ has Arrhenius dependence on T
 If T-dependence in pre-factor is neglected

$$\mu = \mu_0 \exp\left(\frac{E_A}{RT}\right)$$

$$\mu_0 = \frac{RT_m d_0^c}{42 V_m D_{0,V}}$$

Example problem: Couette flow with T-gradient



In absence of viscous dissipation the T-field is independent of the velocity.
 \Rightarrow one way coupling: $v = v(T)$ but $T \neq T(v)$
 Temperature field:

$$\nabla \cdot [v T - \nabla T] = 0 \rightarrow \frac{dT}{dz} = 0 \Rightarrow T = T_B + \frac{\Delta T}{H} z$$

$$\left[\frac{T}{T_B} = 1 + \frac{\Delta T}{T_B} \frac{z}{H} \right] = \underline{1 + b z'} \quad z' = \frac{z}{H} \quad b = \frac{\Delta T}{T_B}$$

Velocity & pressure fields

$$-\nabla \cdot [\mu(T) (\nabla \underline{v} + \nabla^T \underline{v})] + \nabla \pi = 0 \quad \pi = p + \rho g z$$

$$\nabla \cdot \underline{v} = 0$$

clearly $v_z = 0 \rightarrow v_{z,x} = v_{z,z} = 0$

Continuity: $\frac{\partial v_x}{\partial x} + \frac{\partial v_z}{\partial z} = 0 \Rightarrow v_{x,x} = 0$

Deviatoric stress components

$$\underline{\underline{\tau}} = \mu (\nabla \underline{v} + \nabla^T \underline{v}) = \mu \begin{bmatrix} 2v_{x,x} & v_{x,z} + v_{z,x} \\ v_{z,x} + v_{x,z} & 2v_{z,z} \end{bmatrix}$$

$$\underline{\underline{\tau}} = \mu \begin{bmatrix} 0 & v_{x,z} \\ v_{x,z} & 0 \end{bmatrix} = \begin{bmatrix} \tau_{x,x} & \tau_{x,z} \\ \tau_{z,x} & \tau_{z,z} \end{bmatrix}$$

$$\nabla \cdot \underline{\underline{\tau}} = \begin{bmatrix} \tau_{x,xx} + \tau_{x,zz} \\ \tau_{z,xx} + \tau_{z,zz} \end{bmatrix} = \begin{bmatrix} \frac{\partial}{\partial x}(\mu(T) 0) + \frac{\partial}{\partial z}(\mu(T) v_{x,z}) \\ \frac{\partial}{\partial x}(\mu(T) v_{x,z}) + \frac{\partial}{\partial z}(\mu(T) 0) \end{bmatrix}$$

$$\nabla \cdot \underline{\underline{\tau}} = \begin{bmatrix} \frac{\partial}{\partial z}(\mu(T) \frac{\partial v_x}{\partial z}) \\ 0 \end{bmatrix}$$

$$\frac{\partial}{\partial x} [\mu(T(z)) v_{x,z}(z)] = 0$$

$$\nabla \pi = \begin{pmatrix} \pi_{x,x} \\ \pi_{z,z} \end{pmatrix} = \begin{pmatrix} \pi_{x,x} \\ 0 \end{pmatrix}$$

because flow is horizontal

\Rightarrow all terms in z-momentum balance vanish.

$$-\frac{\partial}{\partial z} \left[\mu(T(z)) \frac{\partial v}{\partial z} \right] + \frac{\partial \Pi}{\partial x} = 0 \quad v = v_x$$

General channel flow equation



In Poiseuille (sorry) flow we have x pressure gradient

In Couette flow we don't. $\Rightarrow \frac{\partial \Pi}{\partial x} = 0$

Need to solve following problem

$$\text{ODE: } \frac{d}{dz} \left[\mu(T(z)) \frac{dv}{dz} \right] = 0$$

$$\text{BC: } v(0) = 0 \quad v(H) = v_T$$

$$\text{Const: } \mu = \mu_0 \exp\left(\frac{E}{RT}\right) \quad E_A = E$$

$$T = T_B + \frac{\Delta T}{H} z$$

Integrate once:

$$\mu \frac{dv}{dz} = c_1, \quad \text{where } c_1 = \tau = \text{shear stress}$$

Integrate again

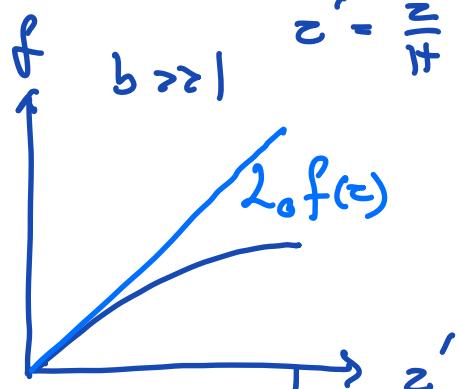
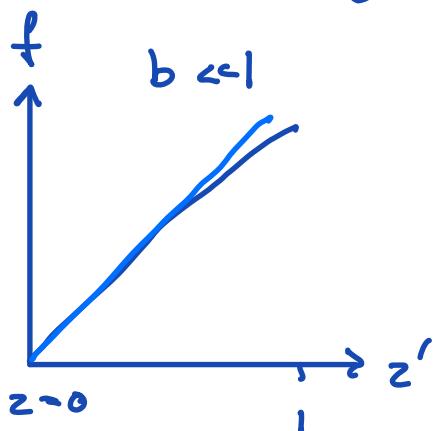
$$v(z) = \tau \int_0^z \frac{dz'}{\mu(T(z'))} = \frac{\tau}{\mu_0} \int_0^z \exp\left(-\frac{E/R}{T(z)}\right) dz$$

$$v(z) = \frac{\tau}{\mu_0} \int_0^z \exp\left(\underbrace{-\frac{E/R}{T_B + \frac{\Delta T}{H} z}}_{f(z)}\right) dz$$

difficult integral, but if $\Delta T \ll T_B$

we can approximate exponential factor

$$f(z) = -\frac{E}{R T_B} \frac{1}{1 + \frac{\Delta T}{T_B} \frac{z}{H}} = \frac{-a}{1 + bz'} \quad a = \frac{E}{R T_B}, \quad b = \frac{\Delta T}{T_B}$$



Almost straight line for $b \ll 1$

Approximate with Taylor series expansion

$$\lambda_0 f(z) = f(0) + \left. \frac{df}{dz'} \right|_0 z' = -a + ab z' = -a(1+bz')$$

$$\frac{df}{dz} = \frac{ab}{(1+bz')^2}$$

so we have

$$f(z) = \frac{-a}{1+bz'} \approx -a(1+bz')$$

$$e^{-a(1+bz')} = e^{-a} e^{+abz'}$$

$$v(z) = \frac{\tau}{\mu_0} e^{-a} \int^z e^{abz'} dz \quad dz = H dz'$$

$$v(z') = \frac{\tau H}{\mu_0} e^{-a} \int_0^{z'} e^{abz''} dz'' = \frac{\tau H}{\mu_0 ab} \frac{e^{-a}}{1} (e^{abz'} - 1)$$

$$v(z') = \frac{\tau H}{\mu_0 ab} (e^{abz'} - 1)$$

1) Set velocity \rightarrow fluid shear stress

2) Set shear stress \rightarrow fluid velocity

our case is (2)

$$v(z'=-1) = v_T = \frac{\tau_{ff}}{\mu_0} \frac{e^{-a}}{ab} (e^{ab} - 1)$$

$$\Rightarrow \bar{v} = \frac{v_T \mu_0}{T \hbar} \frac{ab}{e^{-q}} \frac{1}{e^{ab}-1}$$

substitute

$$\boxed{\frac{v(z')}{v_T} = \frac{e^{abz'} - 1}{e^{ab} - 1}}$$

$$\text{where } a = \frac{E_q}{RT_B} \quad b = \frac{\Delta T}{T_B} \quad z' = \frac{z}{\hbar}$$