

# Derivation of the equation of motion

(1)

Start with the general balance law.

$$\frac{\partial u}{\partial t} + \nabla \cdot j(u) = f_s$$

where  $u$  is the unknown that is balanced,  $j(u)$  is a set of fluxes that transport the unknown and  $f_s$  is a set of source terms.

So far the unknown  $u$  has been a scalar, for example the energy  $u = \rho c_p T$ . Here we will consider an unknown that is a vector which will give the equations a tensorial nature.

The equations of motion are based on Euler's "Principle of linear momentum" which states that: The total force on a body is equal to the rate of change of the total momentum of the body. (1752)

Hence our unknown is the momentum, in particular the linear<sup>\*</sup> momentum,  $\underline{u} = \rho \underline{v}$ , of the body, which is a vector. Here  $\rho$  is the density and  $\underline{v}$  the velocity. Linear momentum is generated within the body by body forces, here we will only consider gravity  $f_s = \rho \underline{\bar{g}}$  where  $\underline{\bar{g}}$  is the gravitational acceleration.

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\* The angular momentum will come into the derivation later.

Now we need to consider the fluxes of linear momentum  $\textcircled{2}$  into and out of a control volume.

a) Advective momentum flux

$$\underline{j}_A = \underline{v} \otimes (\rho \underline{v}) = \rho \underline{v} \otimes \underline{v} = \rho \underline{v} \underline{v}^T$$

this is the linear momentum,  $\rho \underline{v}$ , advected by the velocity of the fluid,  $\underline{v}$ , itself. Hence, the advective momentum flux is inherently non-linear.

Note that  $\underline{j}_A$  is a 2nd order tensor, i.e. a matrix. and  $\otimes$  denotes the outer product as opposed to the inner product.

Inner product:  $\underline{v} \cdot \underline{v} = \underline{v}^T \underline{v} = v_i v_i = v_1 v_1 + v_2 v_2 + v_3 v_3 = \text{scalar}$

outer product:  $\underline{v} \otimes \underline{v} = \underline{v} \underline{v}^T = v_i v_j = \begin{pmatrix} v_1 v_1 & v_1 v_2 & v_1 v_3 \\ v_2 v_1 & v_2 v_2 & v_2 v_3 \\ v_3 v_1 & v_3 v_2 & v_3 v_3 \end{pmatrix}$

b) Diffusive momentum flux:

Linear momentum can enter/exit a control volume even if the flow is parallel to the boundary by momentum diffusion due to shear and normal stresses

$$\underline{j}_D = -\underline{\underline{\sigma}} = - \text{ where } \underline{\underline{\sigma}} = -p\underline{\underline{I}} + \underline{\underline{\tau}} \Rightarrow \underline{j}_D = p\underline{\underline{I}} - \underline{\underline{\tau}}$$

where  $\underline{\underline{\sigma}}$  is the Cauchy stress tensor, which can be decomposed into a volumetric stress,  $-p\underline{\underline{I}}$ , where  $p$  is the pressure of the fluid and the deviatoric stress,  $\underline{\underline{\tau}}$ .

Substituting these expressions into the general balance law we obtain the equations of motion

$$\boxed{\frac{\partial \rho \underline{v}}{\partial t} + \nabla \cdot [\rho \underline{v} \otimes \underline{v} + p \underline{I} - \underline{\underline{T}}] = \rho \underline{g}}$$
 Cauchy Momentum Equation

This equation is very general and is the starting point for all of fluid mechanics. Next we need to complete the model by defining constitutive equations.

### Incompressible Newtonian Fluid

Here we will consider an incompressible Newtonian fluid

For an incompressible fluid  $\nabla \cdot \underline{v} = 0$   $\left( \frac{\partial \rho}{\partial t} + \nabla \cdot (\underline{v} \rho) = 0 \right)$   
 (without source terms)  $\rho = \text{const.}$

For a Newtonian fluid, the deviatoric stress,  $\underline{\underline{T}}$ , depends linearly on the strain rate,  $\underline{\underline{\dot{\epsilon}}}$

$$\boxed{\underline{\underline{T}} = 2\mu \underline{\underline{\dot{\epsilon}}}}$$
 where  $\mu = \text{dynamic viscosity } \left[ \frac{M}{LT} \right]$

rate of strain tensor  $\underline{\underline{\dot{\epsilon}}} = \frac{1}{2} (\nabla \underline{v} + \nabla^T \underline{v})$

where  $\nabla \underline{v} = \begin{pmatrix} \frac{\partial v_1}{\partial x_1} & \frac{\partial v_1}{\partial x_2} & \frac{\partial v_1}{\partial x_3} \\ \frac{\partial v_2}{\partial x_1} & \frac{\partial v_2}{\partial x_2} & \frac{\partial v_2}{\partial x_3} \\ \frac{\partial v_3}{\partial x_1} & \frac{\partial v_3}{\partial x_2} & \frac{\partial v_3}{\partial x_3} \end{pmatrix}$  is the velocity gradient tensor

and  $\nabla^T \underline{v} = (\nabla \underline{v})^T$  is its transpose.

Hence we have the deviatoric and full stress tensors

$$\underline{\underline{\tau}} = \mu (\nabla \underline{v} + \nabla^T \underline{v})$$

$$\underline{\underline{\sigma}} = -p \underline{\underline{I}} + \mu (\nabla \underline{v} + \nabla^T \underline{v})$$

for an Newtonian fluid.

Substituting these expressions into Cauchy's Momentum Equation we obtain

$$\rho \frac{\partial \underline{v}}{\partial t} + \nabla \cdot [\underline{v} \otimes \underline{v} + \frac{p}{\rho} \underline{\underline{I}} - \frac{\mu}{\rho} (\nabla \underline{v} + \nabla^T \underline{v})] = \underline{g} \quad \text{note: } \underline{g} = -g \hat{z}$$

Introduce  $\nu = \frac{\mu}{\rho} \left[ \frac{L^2}{T} \right]$  = kinematic viscosity or momentum diffusivity.

Also  $\frac{1}{\rho} \nabla \cdot (p \underline{\underline{I}}) = \frac{1}{\rho} \nabla p$  we can write

$$\boxed{\frac{\partial \underline{v}}{\partial t} + \nabla \cdot [\underline{v} \otimes \underline{v}] = -\frac{\nabla p}{\rho} + \nabla \cdot [\nu (\nabla \underline{v} + \nabla^T \underline{v})] + \underline{g}}$$

Navier-Stokes equation for variable viscosity  $\nu$ .

In geophysical applications  $\nu$  is strongly dependent on both temperature and strain rate.

For constant viscosity, we can take  $\nu$  out of the divergence and simplify.

$$\nabla \cdot [\nabla \underline{v} + \nabla^T \underline{v}] = \nabla \cdot \nabla \underline{v} + \nabla \cdot (\nabla \cdot \underline{v}) \overset{\text{incompressible}}{=} \nabla^2 \underline{v} \quad \text{"vector Laplacian"}$$

Standard Navier-Stokes equation

$$\boxed{\begin{aligned} \frac{\partial \underline{v}}{\partial t} + \nabla \cdot [\underline{v} \otimes \underline{v}] &= -\frac{\nabla p}{\rho} + \nu \nabla^2 \underline{v} + \underline{g} \quad \& \quad \nabla \cdot \underline{v} = 0 & \text{conservative form} \\ \frac{\partial \underline{v}}{\partial t} + \underline{v} \cdot \nabla \underline{v} &= -\frac{\nabla p}{\rho} + \nu \nabla^2 \underline{v} + \underline{g} \quad \& \quad \nabla \cdot \underline{v} = 0 & \text{convective form} \end{aligned}}$$