

# Energy Conservation Equation

Internal energy: Energy of a body not associated with kinetic or potential energy.

Internal energy ~ thermal energy/ heat  
symbol:  $U$  units: Joule =  $\left[\frac{ML^2}{T^2}\right]$

specific internal energy / energy density

$$u = \frac{U}{m} \quad m = \text{mass} \quad \left[\frac{L^2}{T^2} = \frac{J}{kg}\right]$$

$$\boxed{du = c_p dT} \quad T = \text{temperature}$$

$c_p$  = specific heat capacity

at const. pressure  $\left[\frac{J}{kg K} = \frac{L^2}{T^2 \Theta}\right]$

Physical interpretation:

$c_p$  is the heat required to raise the temperature of 1 kg by 1 degree K.

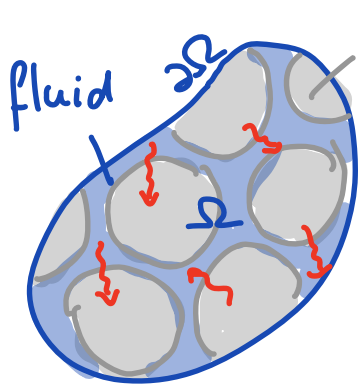
Energy density:

$$u(T) = u_0 + c_p (T - T_0)$$

$u_0$  = ref. energy

$T_0$  = ref. temperature

## Energy of rock-fluid system



Two-phase system  $p \in [r, f]$

$\phi_p$  = volume fraction of phase  $p$

$m_p = \rho_p V_p$  mass of phase  $p$  [M]

$\rho_p$  = density of phase  $p$  [ $\frac{M}{L^3}$ ]

$V_p = \phi_p V$  volume of phase  $p$  [ $L^3$ ]

$\phi = \phi_f$  = porosity

$V = V_f + V_r$  = total volume

Internal energy of rock:

$$U_r = u_r m_r = u_r \rho_r V_r = u_r \rho_r \phi_r V = \int_{\Omega} (1-\phi) \rho_r u_r dV$$

Similarly we have for the fluid

$$U_f = \int_{\Omega} \phi \rho_f u_f dV$$

where  $u_f = u_{0,f} + c_{p,f} (T_f - T_0)$

$$u_r = u_{0,r} + c_{p,r} (T_r - T_0)$$

choosing  $u_{o,r} = u_{o,f} = T_o = 0$

⇒ Internal energy of phases in  $\Omega$

$$U_r = \int_{\Omega} (1-\phi) \rho_r c_{p,r} T_r dV$$

$$U_f = \int_{\Omega} \phi \rho_f c_{p,f} T_f dV$$

Total internal energy of porous medium

$$U_T = U_r + U_f = \int_{\Omega} (1-\phi) \rho_r c_{p,r} T_r + \phi \rho_f c_{p,f} T_f dV$$

Assumption of local thermal equilibrium

$$T_f = T_r = T$$

$$\Rightarrow U_T = \int_{\Omega} \underbrace{[\phi \rho_f c_{p,f} + (1-\phi) \rho_r c_{p,r}]}_e T dV$$

$e$  = total energy density of porous medium  
per unit volume  $\left[ \frac{J}{m^3} = \frac{M}{LT^2} \right]$

General balance equation:  $\frac{\partial u}{\partial t} + \nabla \cdot \underline{j} = \hat{f}_s$

$u = \text{unknown}$ ,  $\underline{j} = \text{flux}$ ,  $\hat{f}_s = \text{source/sink}$

1) Unknown

$$e = (\phi \rho_f c_{p,f} + (1-\phi) \rho_r c_{p,r}) T$$

Note: Conserved quantity!  $\nabla \cdot \underline{j} = 0 \Rightarrow$  no source/sink term

$$\overline{\rho c_p} = \phi \rho_f c_{p,f} + (1-\phi) \rho_r c_{p,r} \Rightarrow e = \overline{\rho c_p} T$$

2) Energy fluxes

a) Conductive heat flux

Fourier's law:  $\underline{j}_c = -\kappa \nabla T$

where  $\kappa = \text{thermal conductivity}$

$$\text{units } \left[ \frac{W}{mK} = \frac{ML}{T^3 \Theta} \right]$$

This applies in each phase:

$$\underline{j}_{c,f} = -\kappa_f \nabla T \quad \underline{j}_{c,s} = -\kappa_s \nabla T$$

Total conductive flux

$$\underline{j}_c = \phi \underline{j}_{c,f} + (1-\phi) \underline{j}_{c,s}$$

$$\underline{j}_c = - [\phi \kappa_f + (1-\phi) \kappa_s] \nabla T$$

mean conductivity:  $\bar{\kappa} = \phi \kappa_f + (1-\phi) \kappa_s$

$$\underline{j}_c = - \bar{\kappa} \nabla T$$

b) advective heat flux

$$\underline{j}_A = \underline{v} \rho u = \underline{v} \rho c_p T$$

applies in each phase

$$\underline{j}_{A,f} = \underline{v}_f \rho_f c_{p,f} T$$

$$\underline{j}_{A,s} = \underline{v}_s \rho_s c_{p,s} T$$

Total advective heat flux

$$\underline{j}_A = \phi \underline{j}_{A,f} + (1-\phi) \underline{j}_{A,s}$$

$$= \phi \underline{v}_f \rho_f c_{p,f} T + (1-\phi) \cancel{\underline{v}_s} \rho_s c_{p,s} T$$

$\uparrow$   
 $q$

$$\Rightarrow \underline{j}_A = q \rho_f c_{p,f} T$$

3, Source/Sink  $\hat{f}_s = 0$

because  $e$  is a conserved quantity

Substitute into the general balance law

$$\overline{\rho c_p} \frac{\partial T}{\partial t} + \nabla \cdot [\underline{v}_f \rho_f c_{p,f} T - \bar{\kappa} \nabla T] = 0$$

If  $\overline{\rho c_p} = \text{const.}$

$$\Rightarrow \frac{\partial T}{\partial t} + \nabla \cdot [\underline{v}_e T - \bar{\alpha} \nabla T] = 0$$

$$\bar{\alpha} = \frac{\bar{\kappa}}{\overline{\rho c_p}} \quad \text{mean thermal diffusivity}$$

$$\underline{v}_e = \underline{v}_f \underbrace{\frac{\phi \rho_f c_{p,f}}{\overline{\rho c_p}}}_{\leq 1}$$

effective velocity of thermal fronts which is less than the fluid velocity because of heat exchange with solid