

Balance Laws

- Most fundamental equations in natural sciences are balance laws or derived from them.
- Balance law accounts for gains and losses of a quantity due to transport and sources/sinks.
- If there are no sinks/sources of a quantity it is a "conserved quantity" and the balance law becomes a conservation law.
- In multi phase systems like porous media
It is not trivially obvious what quantities are conserved (in absence of obvious sources/sinks like wells)
 - Mass of the pore fluid is conserved
 - Energy of the pore-fluid is not conserved
→ because fluid can lose/gain energy to/from grains
 - Total energy of the system is conserved.

Note on units:

In the derivation of conservation laws it is important to ensure the units match. We use general notation:

$L \equiv$ units of length

$N \equiv$ units of number eg mol

$T \equiv$ units of time

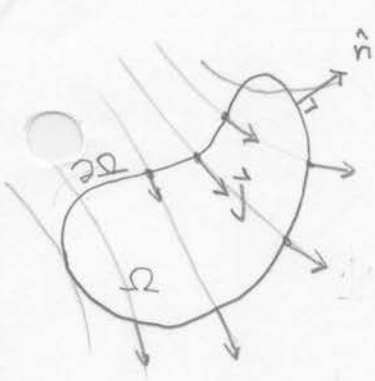
$1 \equiv$ unit less

$M \equiv$ units of mass

$\# \equiv$ arbitrary units "stuff"

Indicate units of a quantity in brackets, e.g., viscosity μ [$\frac{M}{LT}$]

Derivation of general balance law



Account for change of unknown $u(x,t)$ in domain Ω due to fluxes \vec{j} across the boundary $\partial\Omega$ and production/consumption by \hat{f} in Ω .

Units of basic quantities:

- u is a density $[\frac{\#}{L^3}]$.
- \vec{j} is a flux $[\frac{\#}{L^2 T}]$
- \hat{f}_s is a volumetric rate $[\frac{\#}{L^3 T}]$

General balance on Ω : $\boxed{\frac{d}{dt} U = J + F}$

1) U is amount of u in Ω : $U(t) = \int_{\Omega} u(x,t) dV$ $[\#]$

2) J is rate of transport of transport of u across $\partial\Omega$ by \vec{j} : $J(t) = - \oint_{\partial\Omega} \vec{j}(u) \cdot \hat{n} dA$ $[\frac{\#}{T}]$

3) F is rate of production/consumption in Ω of u inside Ω : $F(t) = \int_{\Omega} \hat{f}_s(x,t) dV$ $[\frac{\#}{T}]$

Substitute into balance equation:

$\boxed{\frac{d}{dt} \int_{\Omega} u dV = - \oint_{\partial\Omega} \vec{j}(u) \cdot \hat{n} dA + \int_{\Omega} \hat{f}_s dV}$

Integral balance law

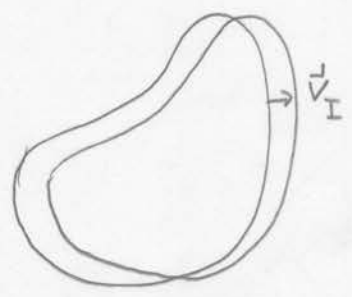
units: $\frac{1}{T} \frac{\#}{L^3} L^3 = \frac{\#}{L^3 T} L^3 = \frac{\#}{L^3 T} L^3$

\Rightarrow each term $[\frac{\#}{T}]$ is rate of change of $\#$!

To obtain a local PDE we need to

- 1) Exchange derivative and integral
- 2) Transform surface to volume integral

1) Reynolds Transport Theorem:



The domain Ω is moving with velocity \vec{v}

$$\frac{d}{dt} \int_{\Omega(t)} u \, dV = \int_{\Omega} \frac{\partial u}{\partial t} \, dV + \oint_{\partial\Omega} u (\vec{v}_I \cdot \hat{n}) \, dS$$

We consider Eulerian limit: of fixed domain $\vec{v}_I = 0 \Rightarrow \frac{d}{dt} \int_{\Omega} u \, dV = \int_{\Omega} \frac{\partial u}{\partial t} \, dV$

2) Divergence theorem: $\oint_{\partial\Omega} \vec{j} \cdot \hat{n} \, dA = \int_{\Omega} \nabla \cdot \vec{j} \, dV$

substitute: $\int_{\Omega} \left(\frac{\partial u}{\partial t} + \nabla \cdot \vec{j}(u) - \hat{f}_s \right) dV = 0$

Since this must hold for any domain $\Omega \forall \Rightarrow$ Integrand = 0

Local form of general balance law

$$\frac{\partial u}{\partial t} + \nabla \cdot \vec{j}(u) = \hat{f}_s$$

- where
- $u = \text{unknown} \quad \left[\frac{\#}{L^3} \right]$
 - $\vec{j}(u) = \text{flux} \quad \left[\frac{\#}{L^2 T} \right]$
 - $\hat{f}_s = \text{vol. rate} \quad \left[\frac{\#}{L^3 T} \right]$