

# Scaling the Navier-Stokes Equations

①

Last time we derived the Navier-Stokes Equations

$$\rho \frac{\partial \underline{v}}{\partial t} + \nabla \cdot [\rho (\underline{v} \otimes \underline{v}) - \mu (\nabla \underline{v} + \nabla^T \underline{v})] = -\nabla p + \rho \underline{g} \quad \& \quad \nabla \cdot \underline{v} = 0$$

As long as we don't consider buoyancy driven flows we can absorb the gravity term into a reduced pressure.

$$-\nabla p + \rho \underline{g} = -\nabla p - \rho g \hat{z} = -\nabla p - \rho g \nabla z = -\nabla (p + \rho g z) = -\nabla \pi$$

where  $\pi = p + \rho g z$  is the reduced pressure.

This can be related to the hydraulic head  $h = \frac{\pi}{\rho g}$  in case you are used to thinking in heads.

Here we leave the NS-eqn in terms of reduced pressure

$$\boxed{\rho \frac{\partial \underline{v}}{\partial t} + \nabla \cdot [\rho (\underline{v} \otimes \underline{v}) - \mu (\nabla \underline{v} + \nabla^T \underline{v})] = -\nabla \pi}$$

First we non-dimensionalize with generic scales to define the standard dimensionless parameters then specialize it to particular cases.

Let's take stock of parameters & variables:

- Dependent variables:  $\underline{v}$ ,  $\pi$  ( $p$ )
- Independent variables:  $\underline{x}$ ,  $t$
- Parameters:  $\rho$ ,  $\mu$  + (geometry, BC's, IC)

We scale variables and parameters functions of the variables

$$\underline{v}' = \frac{\underline{v}}{V_c} \quad \underline{x}' = \frac{\underline{x}}{X_c} \quad t' = \frac{t}{t_c} \quad \pi' = \frac{\pi}{\pi_c} \quad \mu' = \frac{\mu}{\mu_c}$$

$$\Rightarrow \frac{\rho V_c}{t_c} \frac{\partial \underline{v}'}{\partial t'} + \nabla' \cdot \left[ \frac{\rho V_c^2}{X_c} (\underline{v}' \otimes \underline{v}') - \frac{\mu V_c}{X_c^2} \mu' (\nabla' \underline{v}' + \nabla'^T \underline{v}') \right] = -\frac{\pi_c}{X_c} \nabla' \pi'$$

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First, we will rearrange the char. groups into a standard advection diffusion scaling by setting the accumulation term to unity. After dropping the primes we have

$$\frac{\partial \underline{v}}{\partial t} + \underbrace{\nabla \cdot \left[ \frac{v_c t_c}{x_c} (\underline{v} \otimes \underline{v}) \right]}_{\Pi_1} - \underbrace{\frac{\mu t_c}{\rho x_c^2} \mu' (\nabla \underline{v} + \nabla \underline{v}^T)}_{\Pi_2} = \underbrace{\frac{\tau_c t_c}{\rho v_c x_c}}_{\Pi_3} \nabla \tau$$

So that we have 3 dimensionless groups. The first two are identical to those arising in the standard advection diffusion equation. They define advective and diffusive timescales.

$$\Pi_1 = \frac{v_c t_c}{x_c} = 1 \Rightarrow \text{advective time scale: } t_A = \frac{x_c}{v_c}$$

"time for fluid to flow distance  $x_c$ "

$$\Pi_2 = \frac{\mu t_c}{\rho x_c^2} = \frac{\nu_c t_c}{x_c^2} \Rightarrow \text{diffusive time scale: } t_D = \frac{x_c^2}{\nu_c}$$

where  $\nu_c = \frac{\mu}{\rho}$  is the momentum diffusivity  
"time for momentum/vorticity to diffuse distance  $x_c$ "

In our applications  $\Pi_3 = 1$  will be used to define an internal pressure scale  $\tau_c = \rho v_c x_c / t_c$ . But in pressure driven flows, e.g. pipe flows, it could also define a pressure-based time scale  $t_p = \rho v_c x_c / \tau_c$  where  $\tau_c$  would be an external pressure scale.

Choosing a diffusive timescale  $t_c = t_D$  we have.

(3)

$$\frac{\partial \underline{v}}{\partial t} + \nabla \cdot \left[ \frac{v_c x_c}{\nu} (\underline{v} \otimes \underline{v}) - \mu (\nabla \underline{v} + \nabla^T \underline{v}) \right] = \nabla \pi$$

Hence we have one dimensionless group in the form of a Peclet number comparing advection & diffusion of momentum

$$\boxed{Pe_m = \frac{v_c x_c}{\nu} = \frac{\rho v_c x_c}{\mu} = \frac{t_D}{t_A} = Re} \quad \text{Reynolds Number}$$

In fluid mechanics this dimensionless number is called the Reynolds number.

$$\boxed{\frac{\partial \underline{v}}{\partial t} + \nabla \cdot [Re (\underline{v} \otimes \underline{v}) - \mu (\nabla \underline{v} + \nabla^T \underline{v})] = \nabla \pi}$$

Clearly, the momentum term vanishes if  $Re \rightarrow 0$

For our application in viscous flow of ice, i.e. glaciers & ice sheets we have the following parameters:

$$\rho = 10^3$$

$$v_c = 10 \text{--} 100 \text{ m/yr} \approx 10^{-7} \text{--} 10^{-5} \frac{\text{m}}{\text{s}} \sim 10^{-6} \frac{\text{m}}{\text{s}} \quad (\text{yr} \sim 10^7 \text{s})$$

$$\mu_c = 10^{13} \text{--} 10^{15} \text{ Pas} \sim 10^{14} \text{ Pas}$$

$$x_c = 10^2 \text{--} 10^3 \text{ m} \sim 10^2 \text{ m}$$

$$Re = \frac{\rho v_c x_c}{\mu_c} = 10^{3-6+2-14} = 10^{-15}$$

$\Rightarrow$  advective momentum transport is negligible

But is it worth resolving diffusive time scales?

$$t_D = \frac{x_c^2 \rho}{\mu_c} = 10^{4+3-14} \text{ s} = 10^{-7} \text{ s}$$

Very short time scale compared to years to 100 years of glacier response

⇒ Choose a different non-dimensionalization

- clearly the viscosity term is important
- like to get rid of time derivative

⇒ scale to viscous term

$$\frac{\rho v_c}{t_c} \frac{\partial \underline{v}'}{\partial t'} + \nabla' \cdot \left[ \frac{\rho v_c^2}{X_c} (\underline{v}' \otimes \underline{v}') - \frac{\mu_c v_c}{X_c^2} \mu' (\nabla' \underline{v}' + \nabla'^T \underline{v}') \right] = - \frac{\pi_c}{X_c} \nabla' \pi'$$

dropping primes: ↑ divide by fluid to set viscous term to unity

$$\frac{\rho X_c^2}{\mu_c t_c} \frac{\partial \underline{v}}{\partial t} + \nabla \cdot \left[ \underbrace{\frac{v_c X_c}{\nu}}_{Re} (\underline{v} \otimes \underline{v}) - \mu (\nabla \underline{v} + \nabla^T \underline{v}) \right] = - \underbrace{\frac{\pi_c X_c}{\mu_c v_c}}_{=1} \nabla \pi_c$$

choose advective time scale:  $t_c = \frac{X_c}{v_c}$  =1 ⇒  $\pi_c = \frac{\mu_c v_c}{X_c}$

$$Re \left( \frac{\partial \underline{v}}{\partial t} + \nabla \cdot (\underline{v} \otimes \underline{v}) \right) - \nabla \cdot [\mu (\nabla \underline{v} + \nabla^T \underline{v})] = - \nabla \pi$$

limit  $Re \ll 1$  we obtain Stokes equation

$$\nabla \cdot [\mu (\nabla \underline{v} + \nabla^T \underline{v})] = \nabla \pi$$

$$\nabla \cdot \underline{v} = 0$$

Here written for variable viscosity

In the limit of constant viscosity  $\mu' = 1$

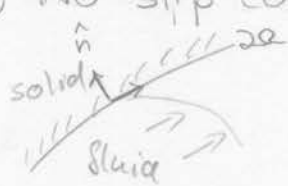
$$\nabla^2 \underline{v} = \nabla \pi$$

$$\nabla \cdot \underline{v} = 0$$

⇒ Stokes/viscous flow is steady, i.e. flow field instantaneously adjust to changes in any forcing or BC.

# Boundary conditions for Stokes Equation

1) No slip condition at solid boundary



is boundary is stationary  $v_b = 0$

$$\underline{v}|_{x \in \partial\Omega} = \underline{0}$$

Dirichlet BC

⇒ prescribe velocity

⇒ implemented with constraints

2) Free slip / No shear stress condition



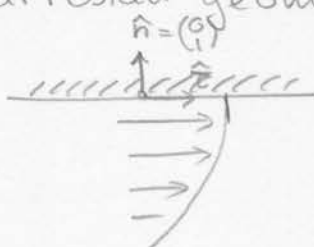
$$\underline{v} \cdot \hat{n}|_{\partial\Omega} = 0 \quad \text{no flow across boundary}$$

$$\hat{t} \cdot (\underline{\underline{\sigma}} \cdot \hat{n})|_{\partial\Omega} = 0 \quad \text{no shear stress}$$

here  $\underline{t} = \underline{\underline{\sigma}} \cdot \hat{n}$  is the traction vector on boundary

$t_{||} = \hat{t} \cdot \underline{t}$  component of traction parallel to boundary (shear stress)

In cartesian geometry:  $\hat{n} = \begin{pmatrix} 0 \\ 1 \end{pmatrix}$   $\hat{t} = \begin{pmatrix} 1 \\ 0 \end{pmatrix}$



$$\hat{t} \cdot (\underline{\underline{\sigma}} \cdot \hat{n}) = (1 \ 0) \cdot \begin{pmatrix} \sigma_{xx} & \frac{1}{2}(\sigma_{xy} + \sigma_{yx}) \\ \frac{1}{2}(\sigma_{xy} + \sigma_{yx}) & \sigma_{yy} \end{pmatrix} \cdot \begin{pmatrix} 0 \\ 1 \end{pmatrix} = \frac{1}{2}(\sigma_{xy} + \sigma_{yx})$$

since  $v_y = 0$  along but  $\frac{\partial v_y}{\partial x} = 0$

$$\Rightarrow \frac{\partial v_x}{\partial y} |_{\partial\Omega} = 0 \quad \text{Neumann BC}$$

$$\text{more generally } \boxed{\nabla(\underline{v} \cdot \hat{t}) \cdot \hat{n} = 0}$$

Note: We don't need to impose BC's on the (reduced) pressure!

This is not trivially obvious, but can be demonstrated

by showing that the pressure is a Lagrange multiplier that enforces incompressibility.